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CHARACTERISTICS OF THE TURBULENT  
BOUNDARY LAYER WITH HEAT AND MASS  
TRANSFER: DATA TABULATION

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**Aerodynamics Research Report No. 280**

**CHARACTERISTICS OF THE TURBULENT BOUNDARY LAYER WITH HEAT  
AND MASS TRANSFER: DATA TABULATION**

**by**

**James E. Danberg**

**ABSTRACT: A tabulation of turbulent boundary layer data obtained under conditions of heat and mass transfer at a Mach number of 6.7 is presented. The report supplements the treatise given in NOLTR 64-99. A brief description of the model and test procedure is included.**

**U. S. NAVAL ORDNANCE LABORATORY  
White Oak, Silver Spring, Maryland**

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**Characteristics of the Turbulent Boundary Layer with Heat and Mass Transfer: Data Tabulation**

This report presents the measured and deduced data obtained during an extensive investigation of hypersonic turbulent boundary layers with heat and mass transfer. The work was sponsored by the Bureau of Naval Weapons under Task No. RMGA-42-034/212-1/F009-10-001. It resulted in a Ph.D. thesis by the author submitted to the Catholic University of America. Only summary data were included in the thesis, which was also published as NOLTR 64-99. The present report was compiled after numerous requests for detailed data from other researchers in this field.

The author wishes to acknowledge the efforts of the Aerophysics Division of the U. S. Naval Ordnance Laboratory in preparing the material for publication.

E. F. SCHREITER  
Captain, USN  
Commander



E. L. HARRIS  
By direction

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LIST OF SYMBOLS

$C_f$	skin friction coefficient, $\tau_w / \frac{1}{2} \rho_\infty u_\infty^2$
$C_{f0}$	skin friction coefficient for zero mass transfer
$C_q$	mass transfer coefficient, $\rho_w v_w / \rho_\infty u_\infty$
$M$	local Mach number
$M_\delta$	Mach number at outer edge of boundary layer
$P_\infty$	supply air pressure
$Re_x$	Reynolds number, $\rho_\infty u_\infty x / \mu_\infty$
$Re_\delta$	Reynolds number, $\rho_\infty u_\infty \delta / \mu_\infty$
$St$	Stanton number
$St_0$	Stanton number for zero mass transfer
$T_\infty$	supply air temperature
$T_w$	wall surface temperature
$T_\delta$	temperature at outer edge of boundary layer
$u$	local velocity
$u_\delta$	velocity at outer edge of boundary layer
$v_w$	velocity component perpendicular to wall at wall surface
$x$	distance from leading edge of plate in direction of free-stream velocity
$\delta$	total boundary layer thickness
$\delta^*$	displacement thickness
$\theta$	momentum thickness
$\theta$	energy thickness
$\mu_\infty$	viscosity at outer edge of boundary layer
$\rho_w$	density at wall condition
$\rho_\infty$	density at outer edge of boundary layer
$\tau_w$	wall shear stress

## INTRODUCTION

NOLTR 64-99 (ref. (1)) summarized an extensive program of turbulent boundary layer measurements under conditions of heat and mass transfer at a Mach number of 6.7. That report contained some typical velocity and temperature profiles as well as the correlation of the boundary layer profiles in terms of a number of parameters related to the heat and mass transfer, etc. In order to make that report more generally useful, it has been decided to publish in the present report the tabulated boundary layer data obtained during the course of that project.

The experiments were performed in the U. S. Naval Ordnance Laboratory's Hypersonic Research Tunnel using a Mach number 6.7 uniform flow two-dimensional nozzle with an exit area of about  $25 \times 25 \text{ cm}^2$ . The supply pressure and temperature were held constant during each test at a fixed pressure value between 15 and 38 atmospheres and at a constant supply temperature of  $550^\circ\text{K}$ . The control of these conditions limited the average deviation in nozzle temperature to  $\pm 1^\circ\text{C}$  and in supply pressure to  $\pm 0.1$  atmosphere.

The boundary layer measurements were made on a porous flat plate (see figure 1) which spanned the wind tunnel test section with the testing surface in the plane of symmetry of the two-dimensional nozzle. The plate had a sharp leading edge (radius of about .015 mm) and it had a smooth (about 11 microinches) continuous surface. Inserted in the testing surface of the model was a porous plate about 49 cm long, 18 cm wide, and 1.0 cm thick. The porous plate was made of 316 stainless steel powder sintered into compact material with a density of about 43 percent of solid stainless steel. Further details are given in the original report.

In order to make this tabulation of the experimental data more useful and complete, the instrumentation employed and the data reduction techniques are summarized in the following sections.

## INSTRUMENTATION AND DATA REDUCTION

### Pitot Pressure Probes

The majority of boundary layer Pitot pressure surveys were made using circular stainless steel tubing .559 mm in outside diameter and with an inlet diameter of .254 mm. A few surveys were made using rectangular cross section probes made from crushed tubing. Circular probes were preferred because of the greater ease in determining their position and orientation with respect to the model.

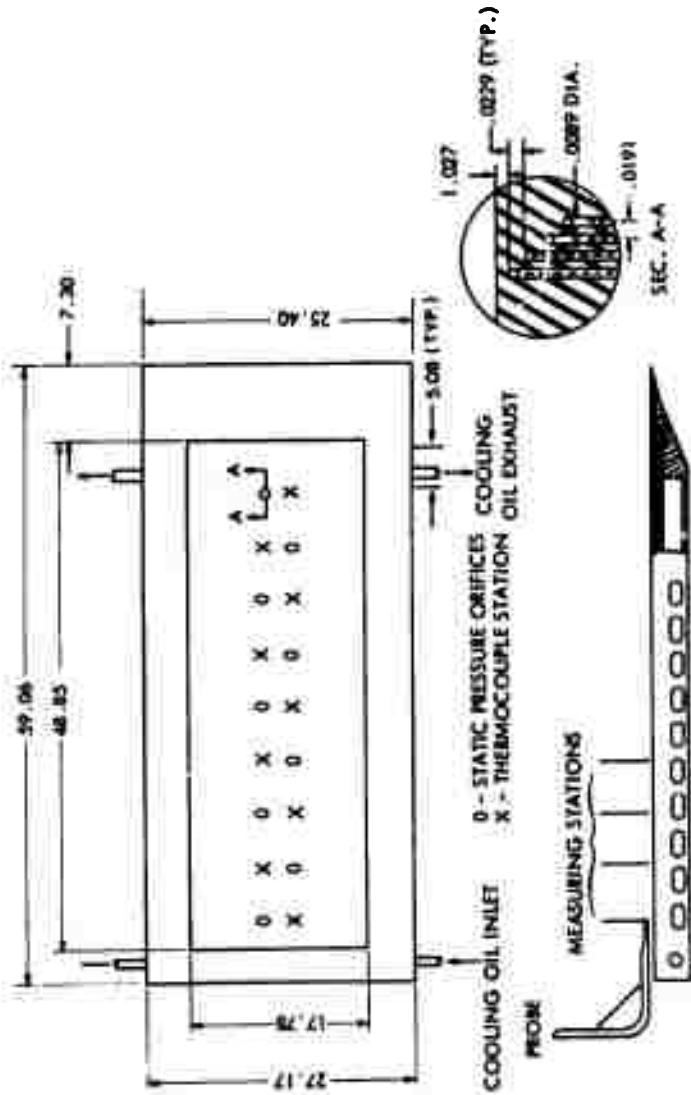


FIG. 1 SKETCH OF MODEL ( ALL DIMENSIONS IN CM )

Pressures were measured with transducers with ranges of 0-1 atmosphere or 0-300 mmHg. Transducers and recording systems were calibrated, before and after each survey, against a mercury manometer with  $\pm 1$  mm measuring accuracy.

The probes were held in the tunnel by a micrometer-traversing mechanism which allowed positioning of the probe with an accuracy of .025 mm. Each traverse was made from the free stream toward the plate. Wall contact, used to evaluate absolute distances from the wall, was indicated by the completion of an electric circuit.

#### Pressure Data Reduction

The NACA tables (ref. (2)) were used to compute the Mach number from the measured Pitot pressure and the static pressure which was assumed constant across the boundary layer and equal to the measured wall static pressure. Wall static pressures were measured by orifices in the porous plate surface through which stainless steel tubing (0.635 mm I.D.) was inserted flush with the testing surface. An oil manometer was used to measure the static pressure with an accuracy of  $\pm 1$  percent.

The surface shear stress was calculated by taking the slope of the Mach number distribution at the wall and multiplying this by the velocity of sound and viscosity of air evaluated at the measured wall temperature. The wall temperature and heat flux were obtained from temperature measurements made with iron-constantan thermocouples imbedded in the porous material at each test station. Four thermocouples were located at each station at various depths from the surface. The thermocouple nearest the surface was 1.27 mm beneath the surface. Together with the known location of the others, extrapolation of the temperature distribution to a surface value was felt to give reliable results.

#### Temperature Measurements

The equilibrium temperature probe (ref. (3)) was developed to measure the boundary layer temperature profiles for these experiments. It consists of a 10 degree angle cone of platinum supported by a good thermal insulator. The cone is mounted on the traversing mechanism with its axis parallel to the flow direction. A thermocouple measured the temperature of the cone which ideally should equal the adiabatic wall temperature. Sufficient run time was available in the NOL Hypersonic Tunnel to allow the probe to come into thermal equilibrium before each measurement was made. A second thermocouple in the ceramic insulator allowed the measured cone temperature to be corrected for conduction losses. The data were recorded on strip chart recorders which made continuous monitoring of the temperatures possible.

#### Temperature Probe Data Reduction

A recovery factor for the probe was computed for each survey while the probe was in the free stream where the flow and temperature



conditions were accurately known. It was assumed that the recovery factor remained constant thereafter for that survey. Thus it was possible to calculate the local total temperature in the boundary layer from the cone adiabatic wall temperature measurement, the assumed recovery factor and measured Mach number. Since temperatures were not always measured at the same location as the pressures, an interpolation was made between temperature data points to obtain the temperatures corresponding to the Mach number data points.

Heat transfer rates to the model surface were calculated from the slope of the total temperature distribution interpolated to the surface temperature and the thermal conductivity of air. This procedure supplements the heat transfer obtained from the temperature distribution within the model wall.

In calculating Stanton numbers, the adiabatic wall temperatures are required to obtain the latter for the zero mass transfer cases. It was assumed that the recovery factor equals the Prandtl number raised to the one third power where wall temperature was used to evaluate the Prandtl number. In the mass transfer cases the recovery factor ratios (i.e., recovery factor with mass transfer divided by the zero mass transfer recovery factor) obtained by Leadon and Bartle (ref. (4)) were used.

#### TEST CONDITIONS

As indicated earlier, the tests were run using a nominal Mach number 6.7 nozzle. However, local Mach numbers at the boundary layer edge were somewhat less because of leading edge shock wave losses and boundary layer flow field interaction; the latter was a significant effect in the mass transfer cases. The supply temperature was held constant at 550°K, while the supply pressure was varied between 15 and 38 atmospheres. Thus, the unit Reynolds number varied from 8 to  $19 \times 10^6$  per meter.

Four locations on the model were investigated: 37.78, 42.86, 47.94, and 53.02 cm from the leading edge. Natural transition was believed to have been completed because a local maximum in the wall temperature was observed at or before 32.7 cm from the leading edge. (Reynolds number =  $2.6 \times 10^6$ ). Three wall temperature ratios ( $T_w/T_\infty$ ) were investigated which had numerical values that averaged to 4.1, 5.2, and 7.6. The boundary layers were surveyed at zero air injection and at three mass transfer rates which were approximately equal to 0.09, 0.17, and 0.25 percent of free-stream mass flow per unit area except in the high supply pressure cases where the maximum injection rate was about 0.11 percent of the free-stream mass flow.

#### ARRANGEMENT OF TABLES

The measured and deduced boundary layer data are presented as summary tables containing the detailed profile data. Two summary

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tables precede each set of profile data obtained for specific test conditions, i.e.,  $P_O$ , and  $T_W/T_O$ , and various values of  $C_q$ , as shown in the following tabulation.

Table No.	$P_O^*$ atm	$T_W/T_O^*$	$C_q^*$	Profile Data Table Nos.
1 & 2	15	4.1	0 9.09 x 10 <sup>-4</sup> 17.0 x 10 <sup>-4</sup> 25.0 x 10 <sup>-4</sup>	3 through 23
24 & 25	15	5.2	0 8.77 x 10 <sup>-4</sup> 17.2 x 10 <sup>-4</sup> 24.6 x 10 <sup>-4</sup>	26 through 42
43 & 44	15	7.6	0 8.68 x 10 <sup>-4</sup> 16.2 x 10 <sup>-4</sup> 24.4 x 10 <sup>-4</sup>	45 through 52
53 & 54	38	7.6	0 3.7 x 10 <sup>-4</sup> 7.25 x 10 <sup>-4</sup> 10.13 x 10 <sup>-4</sup>	55 through 58
59 & 60	38	4.1	0 4.12 x 10 <sup>-4</sup> 8.17 x 10 <sup>-4</sup> 12.1 x 10 <sup>-4</sup>	61 through 67

\*The values of  $P_O$ ,  $T_W/T_O$ , and  $C_q$  are average or nominal values for these quantities for the purpose of identifying the tables--the precise values are listed in the tables for each of the surveys carried out.

**REFERENCES**

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- (3) Danberg, J. E., "The Equilibrium Temperature Probe: A Device for Measuring Temperatures in Hypersonic Boundary Layers," The Second National Symposium on Hypervelocity Techniques at the University of Denver, Denver, Colorado, 20-21 Mar 1962
- (4) Leadon, B. M., and Bartle, E. R., "Experimental Evaluation of Heat Transfer with Transpiration Cooling in a Turbulent Boundary Layer at Mach 3.2," J. Aero/Space Sciences, Vol 27, No. 1, 1960, p. 78

TABLE 1 SUMMARY OF SKIN FRICTION AND HEAT TRANSFER DATA,  $T_e/T_g = 4.1$  $T_e/T_g = 4.1$ 

RUN	X mm	NO	$P_a$ atm	$Re_x \times 10^{-6}$	$Re_\theta$	$T_e/T_g$	$C_f \times 10^4$	$C_f/C_{f0}$	$2C_h/C_{f0}$	$St \times 10^6$	$\frac{St}{St_0}$
$C_{f0} = 0$											
$T_e/T_g = 4.48$											
1	377.8	6.60	15.18	3.255	1947	4.475	0	14.58	1.000	0	4.97 1.000
2	428.6	6.55	15.15	3.533	2374	4.480	0	13.85	1.000	0	4.97 1.000
3	479.4	6.54	15.15	3.880	2527	4.479	0	14.46	1.000	0	5.27 1.000
4	530.2	6.49	15.20	4.220	3037	4.490	0	13.36	1.000	0	4.29 1.000
$C_{f0} = 9.09 \times 10^{-4}$											
$T_e/T_g = 4.17$											
5	377.8	6.38	15.15	2.925	3206	4.102	9.23	12.53	.859	1.266	4.23 .537
6	428.6	6.49	15.22	3.446	4028	4.132	9.07	11.45	.827	1.310	4.09 .551
7	479.4	6.60	15.15	4.160	4898	4.263	8.85	9.60	.684	1.223	3.60 .482
8	530.2	6.48	15.22	4.261	5288	4.167	9.21	8.39	.628	1.379	3.17 .501
$C_{f0} = 17.0 \times 10^{-4}$											
$T_e/T_g = 3.94$											
9	377.8	6.39	15.17	3.249	4919	4.102	16.86	5.36	.368	2.312	2.65 .337
10	479.4	6.42	15.12	3.950	6081	3.991	16.24	5.37	.371	2.246	2.57 .344
11	530.2	6.37	15.18	4.264	7511	3.808	17.81	5.17	.387	2.670	1.90 .300
$C_{f0} = 25.0 \times 10^{-4}$											
$T_e/T_g = 3.73$											
12	377.8	6.28	15.15	3.185	6517	3.864	24.91	3.50	.240	3.416	1.96 .249
13	428.6	6.20	15.15	3.619	8156	3.640	24.52	3.07	.222	3.540	1.32 .178
14	479.4	6.22	15.15	3.945	8450	3.759	24.90	3.36	.232	3.440	1.68 .225
15	530.2	6.22	15.22	4.298	10166	3.662	25.80	3.40	.254	3.860	1.29 .204
$C_{f0} = 0$											
$T_e/T_g = 4.31$ (Repeat Run)											
16	377.8	6.52	15.15	3.057	1716	4.418	0	14.29	1.000	0	7.87 1.000
17	428.6	6.32	15.15	3.163	1993	4.171	0	15.30	1.000	0	7.42 1.000
18	479.4	6.44	15.18	3.679	2347	4.346	0	15.47	1.000	0	7.46 1.000
19	530.2	6.45	15.15	4.260	3023	4.297	0	12.54	1.000	0	6.33 1.000
$C_{f0} = 0$											
$T_e/T_g = 4.12$											
20	479.2	6.68	20.05	5.356	3296	4.381	0	11.86	1.000	0	6.16 1.000
21	479.4	6.41	24.95	5.997	3891	4.116	0	9.46	1.000	0	5.30 1.000

TABLE 2 SUMMARY OF BOUNDARY LAYER PARAMETERS,  $T_e/T_A = 4.1$

RUN	X	$R_0 \times 10^{-6}$	$T_e/T_B$	$C_q \times 10^{-4}$	$T_e/T_B = 4.1$					$R\theta$	$\frac{\delta^*}{\theta}$
					$C_q = 0$	$\theta$	$\delta^*$	$\delta$	$\theta$		
$T_e/T_B = 4.48$											
1	377.8	3.255	4.475	0	.226	3.18	5.4	.238	1947	14.07	
2	428.6	3.533	4.480	0	.288	3.66	7.45	.460	2374	12.71	
3	479.4	3.880	4.479	0	.312	4.10	8.0	.464	2527	13.12	
4	530.2	4.220	4.490	0	.382	4.84	9.2	.644	3037	12.67	
$C_q = 9.09 \times 10^{-4}$ $T_e/T_B = 4.17$											
5	377.8	2.925	4.102	9.23	.414	4.82	8.8	.686	3206	11.64	
6	428.6	3.446	4.132	9.07	.501	5.72	10.8	.848	4028	11.42	
7	479.4	4.160	4.263	8.85	.541	6.81	12.0	.753	4698	12.59	
8	530.2	4.261	4.167	9.21	.658	7.86	14.1	1.070	5288	11.94	
$C_q = 17.0 \times 10^{-4}$ $T_e/T_B = 3.94$											
9	377.8	3.249	4.102	16.86	.572	7.68	12.1	.792	4919	13.43	
10	479.4	3.950	3.991	16.24	.738	9.62	15.5	1.070	6081	13.04	
11	530.2	4.264	3.808	17.81	.934	10.70	18.0	1.580	7511	11.46	
$C_q = 25.0 \times 10^{-4}$ $T_e/T_B = 3.73$											
12	377.8	3.185	3.864	24.91	.773	9.96	14.8	1.216	6517	12.88	
13	428.6	3.619	3.640	24.52	.966	11.20	17.3	1.640	8156	11.59	
14	479.4	3.945	3.759	24.90	1.027	12.90	19.7	1.650	8450	12.56	
15	530.2	4.298	3.662	25.80	1.250	14.20	22.7	2.250	10166	11.36	
$C_q = 0$ $T_e/T_B = 4.31$											
16	377.8	3.057	4.418	0	.212	3.14	5.3	.256	1716	14.81	
17	428.6	3.163	4.171	0	.270	3.64	6.7	.272	1993	13.48	
18	479.4	3.679	4.346	0	.306	4.42	8.1	.316	2349	14.44	
19	530.2	4.260	4.297	0	.376	5.68	10.0	.384	3023	15.11	
$C_q = 0$ $T_e/T_B = 4.12$											
20	479.4		4.381	0	.295	4.34	7.9	.352	3296	14.71	
21	479.4		4.116	0	.311	4.30	7.9	NC	3891	13.83	

TABLE 3 - Run 1

$M_0 = 6.60$   
 $Re\theta = 1.947$   
 $\frac{P}{T_0} = 4.475$   
 $Cq = 0$   
 $P_0 = 15.18 \text{ atm}$   
 $T_0 = 546 \text{ }^\circ\text{K}$   
 $T_0 = 56.4 \text{ }^\circ\text{K}$   
 $U_0 = 994.31 \text{ m/sec}$

Y (mm)	M	$T/T_0$	$U/U_0$
14.60	6.60	1.000	1.000
13.33	6.60	1.000	1.000
12.06	6.60	1.000	1.000
10.79	6.57	1.007	.999
9.52	6.55	1.015	.999
8.25	6.47	1.039	.999
7.06	6.40	1.043	.999
6.42	6.28	1.097	.997
5.79	6.11	1.151	.993
5.15	5.88	1.228	.986
4.52	5.55	1.346	.975
3.88	5.15	1.515	.940
3.25	4.73	1.727	.917
2.61	4.29	1.990	.907
2.36	4.16	2.091	.876
2.11	3.98	2.117	.882
1.85	3.83	2.316	.883
1.60	3.67	2.407	.883
1.34	3.53	2.438	.874
1.09	3.30	2.487	.877
.838	2.99	2.541	.871
.582	2.35	2.972	.814
.328	1.46	3.813	.614
.270	1.395	3.830	.614

TABLE 4 - Run 2

$M_0 = 6.55$   
 $Re\theta = 2.374$   
 $\frac{P}{T_0} = 4.480$   
 $Cq = 0$   
 $P_0 = 15.150 \text{ atm}$   
 $T_0 = 546 \text{ }^\circ\text{K}$   
 $T_0 = 57.2 \text{ }^\circ\text{K}$   
 $U_0 = 992 \text{ m/sec}$

Y (mm)	M	$T/T_0$	$U/U_0$
14.94	6.55	1.000	1.000
12.40	6.55	1.000	1.000
9.86	6.49	1.017	1.000
9.23	6.45	1.031	1.000
8.59	6.37	1.052	.998
7.96	6.25	1.086	.995
7.32	6.11	1.130	.991
6.69	5.91	1.188	.977
6.05	5.70	1.263	.967
5.42	5.44	1.355	.955
4.78	5.15	1.472	.940
4.15	4.85	1.608	.923
3.51	4.55	1.766	.905
2.88	4.25	1.942	.884
2.24	3.96	2.140	.854
1.61	3.62	2.382	.829
.927	3.12	2.430	.764
.660	2.90	2.526	.704
.533	2.59	2.733	.655
.406	2.12	3.178	.577
.279	1.63	3.664	.477
.279	1.44	3.854	.430
.279	1.37	3.829	.409

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TABLE 5 - Run 3

$M_0 = 6.54$   
 $Re_0 = 2527$   
 $T_0 = 4.579$   
 $C_1 = 0$   
 $P_0 = 15.15 \text{ atm}$   
 $T_c = 546^\circ \text{K}$   
 $T_0 = 57.3^\circ \text{K}$   
 $U_0 = 992 \text{ m/sec}$

Y (mm)	M	$T/T_0$	$W/W_0$
16.13	6.54	1.000	1.000
13.59	6.52	1.004	1.000
12.32	6.50	1.012	1.000
11.05	6.46	1.025	1.000
9.78	6.38	1.047	.999
8.14	6.31	1.069	.998
6.00	6.11	1.128	.992
4.98	5.81	1.224	.985
3.48	5.63	1.286	.977
2.97	5.43	1.360	.968
2.46	5.22	1.440	.959
1.95	5.01	1.534	.949
1.44	4.77	1.645	.937
1.34	4.54	1.765	.923
1.22	4.44	1.823	.917
1.10	4.09	2.069	.895
1.00	3.87	2.201	.879
1.00	3.63	2.389	.858
1.00	3.48	2.498	.842
1.14	3.18	2.546	.822
1.02	3.01	2.621	.808
.889	2.91	2.630	.787
.762	2.64	2.791	.721
.635	2.36	2.981	.674
.508	1.98	3.323	.622
.381	1.36	4.034	.553
.279	1.12	4.210	.426
			.353

TABLE 6 - Run 4

$M_0 = 6.49$   
 $Re_0 = 3037$   
 $T_0 = 4.490$   
 $U_0 = 990 \text{ m/sec}$   
 $P_0 = 15.20 \text{ atm}$   
 $T_c = 546^\circ \text{K}$   
 $T_0 = 57.9^\circ \text{K}$

Y (mm)	M	$T/T_0$	$W/W_0$
16.26	6.49	1.000	1.000
14.99	6.47	1.005	1.000
13.72	6.42	1.021	1.000
12.45	6.36	1.040	.999
11.18	6.25	1.074	.998
9.91	6.07	1.130	.994
8.64	5.81	1.211	.986
7.37	5.46	1.333	.972
6.10	5.03	1.506	.950
4.83	4.56	1.727	.923
3.56	4.07	2.012	.890
2.29	3.57	2.377	.848
2.03	3.47	2.458	.838
1.78	3.34	2.553	.822
1.27	3.16	2.560	.778
1.02	2.92	2.584	.724
.762	2.61	2.712	.661
.508	1.97	3.242	.546
.279	1.17	4.074	.363

TABLE 7 - Run 5

$$\begin{aligned}
 M_B &= 6.36 \\
 Re_B &= 3206 \\
 \frac{D_V}{B} &= 4.102 \\
 P_0 &= 15.15 \text{ atm} \\
 T_c &= 548 \text{ }^\circ\text{K} \\
 T_B &= 60.4 \text{ }^\circ\text{K} \\
 U_B &= 994 \text{ m/sec}
 \end{aligned}$$

Y (cm)	M	$T/T_B$	$U/U_B$
10.83	6.38	1.000	1.000
10.19	6.31	1.020	.999
9.56	6.18	1.059	.997
8.92	6.01	1.109	.992
8.29	5.80	1.175	.986
7.65	5.54	1.262	.976
7.02	5.23	1.370	.963
6.38	4.93	1.495	.947
5.75	4.63	1.639	.920
5.11	4.33	1.800	.910
4.48	4.01	1.984	.886
3.84	3.76	2.156	.865
3.21	3.50	2.351	.841
2.57	3.27	2.536	.816
1.94	3.02	2.754	.786
1.30	2.71	2.879	.722
.668	2.14	2.994	.581
.414	1.58	3.427	.459
.279	1.13	3.574	.334

TABLE 8 - Run 6

$$\begin{aligned}
 M_B &= 6.49 \\
 Re_B &= 4.028 \\
 \frac{D_V}{B} &= 4.132 \\
 P_0 &= 15.22 \text{ atm} \\
 T_c &= 548 \text{ }^\circ\text{K} \\
 T_B &= 58.1 \text{ }^\circ\text{K} \\
 U_B &= 992 \text{ m/sec}
 \end{aligned}$$

Y (cm)	M	$T/T_B$	$U/U_B$
19.94	6.49	1.000	1.000
13.59	6.45	1.011	.999
12.95	6.42	1.022	.999
12.32	6.36	1.038	.998
11.68	6.27	1.064	.996
11.05	6.15	1.099	.993
10.41	6.02	1.138	.986
9.78	5.83	1.197	.982
9.14	5.63	1.261	.974
8.51	5.41	1.342	.965
7.87	5.10	1.430	.953
7.24	4.93	1.537	.941
6.60	4.68	1.652	.926
5.97	4.42	1.781	.909
5.33	4.20	1.907	.892
4.70	3.96	2.051	.873
4.06	3.74	2.196	.853
3.43	3.49	2.381	.829
2.79	3.27	2.551	.804
2.16	3.08	2.698	.778
1.52	2.76	2.835	.727
1.27	2.63	2.976	.699
1.02	2.42	3.039	.649
.762	2.15	3.055	.579
.508	1.71	3.286	.476
.361	1.41	3.538	.408
.279	1.15	3.737	.341



TABLE 10 - Run 8

$M = 6.48$   
 $Re = 5,288$   
 $\frac{D}{T} = 4.167$   
 $C = 9.21 \cdot 10^{-4}$   
 $P = 15.22 \text{ atm}$   
 $T = 548 \text{ K}$   
 $T = 58.3 \text{ K}$   
 $U = 992 \text{ m/sec}$

$Y$ (mm)	$M$	$T/T_0$	$U/U_0$
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20.09	6.48	1.000	1.000
18.52	6.47	1.001	1.000
17.35	6.40	1.022	999
16.28	6.29	1.055	997
15.01	6.14	1.100	994
13.74	5.93	1.167	988
12.47	5.63	1.267	978
11.20	5.31	1.380	963
9.91	4.95	1.529	945
8.64	4.58	1.703	922
7.37	4.25	1.873	897
6.12	3.84	2.120	864
4.83	3.46	2.394	826
3.51	3.07	2.708	780
2.21	2.61	3.059	721
1.676	2.49	3.165	684
1.295	2.29	3.212	644
1.041	2.14	3.185	591
.787	1.88	3.229	527
.533	1.60	3.706	417
.406	1.093	3.966	337
.279	.916	4.012	.283

TABLE 9 - Run 7

$M_0 = 6.60$   
 $Re_0 = 4698$   
 $\frac{D}{T} = 4.263$   
 $C = 5.85 \cdot 10^{-4}$   
 $P_0 = 15.15 \text{ atm}$   
 $T_0 = 547 \text{ K}$   
 $T_0 = 56.1 \text{ K}$   
 $U_0 = 997 \text{ m/sec}$

$Y$ (mm)	$M$	$T/T_0$	$U/U_0$
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18.69	6.60	1.000	1.000
16.15	6.55	1.013	1.000
14.85	6.48	1.015	1.000
13.61	6.36	1.070	997
12.34	6.15	1.135	993
11.71	6.01	1.179	989
11.07	5.84	1.238	984
10.44	5.64	1.306	978
9.804	5.47	1.368	969
8.534	5.25	1.459	961
7.899	5.03	1.553	949
7.264	4.81	1.653	925
6.639	4.59	1.768	898
5.984	4.38	1.881	864
5.359	4.15	2.017	826
4.724	3.94	2.157	780
4.089	3.72	2.314	721
3.454	3.51	2.472	684
2.819	3.28	2.643	644
2.184	2.82	2.961	591
1.549	2.58	3.120	527
.914	2.13	3.289	417
.640	1.77	3.381	337
.406	1.29	3.586	.508
.279	.915	3.815	.287
	1.10	3.967	.333

TABLE 12 - Run 10

$M = 6.422$   
 $P_0 = 15.12 \text{ atm}$   
 $R_{\theta} = 6.081$   
 $T_c = 547 \text{ }^\circ\text{K}$   
 $T_g = 59.1 \text{ }^\circ\text{K}$   
 $U_g = 990 \text{ m/sec}$   
 $C_q = 16.24 \times 10^{-4}$

$Y$ (cm)	$M$	$T/T_g$	$U/U_g$
21.23	6.42	1.000	1.000
19.96	6.38	1.010	.999
18.69	6.32	1.032	.999
17.42	6.20	1.070	.998
16.79	6.12	1.095	.997
16.15	6.02	1.126	.993
15.52	5.89	1.166	.990
14.88	5.75	1.212	.986
14.25	5.50	1.264	.979
13.61	5.41	1.331	.972
12.98	5.22	1.404	.964
12.34	5.04	1.482	.955
11.71	4.84	1.570	.944
11.07	4.63	1.666	.930
10.44	4.43	1.765	.916
9.804	4.23	1.873	.901
9.169	4.03	1.996	.886
8.534	3.82	2.132	.869
7.899	3.64	2.281	.849
7.264	3.44	2.395	.829
6.629	3.27	2.522	.808
5.994	3.05	2.714	.782
5.359	2.87	2.880	.757
4.724	2.71	3.023	.734
4.089	2.49	3.255	.699
3.454	2.37	3.333	.673
2.815	2.15	3.587	.634
2.184	1.92	3.848	.588
1.930	1.86	3.897	.570
1.676	1.77	3.934	.546
1.422	1.65	3.954	.513
1.168	1.50	4.004	.468
.914	1.34	3.980	.424
.660	1.10	4.091	.348
.406	.716	4.266	.279
.279	.534	4.216	.171

TABLE 11 - Run 9

$M_g = 6.39$   
 $P_0 = 15.17 \text{ atm}$   
 $R_{\theta} = 4.919$   
 $T_c = 546 \text{ }^\circ\text{K}$   
 $T_g = 59.5 \text{ }^\circ\text{K}$   
 $U_g = 989 \text{ m/sec}$   
 $C_q = 16.86 \times 10^{-4}$

$Y$ (cm)	$M$	$T/T_g$	$U/U_g$
20.55	6.39	1.000	1.000
14.20	6.29	1.030	.998
12.93	6.06	1.099	.994
11.66	5.72	1.216	.987
10.39	5.26	1.397	.973
9.75	5.01	1.505	.962
9.12	4.93	1.526	.952
8.48	4.48	1.749	.928
7.85	4.22	1.898	.909
7.21	3.95	2.067	.887
6.58	3.71	2.228	.865
5.94	3.46	2.412	.839
5.31	3.22	2.599	.813
4.67	2.99	2.814	.783
4.037	2.76	3.027	.751
3.402	2.57	3.216	.721
2.767	2.36	3.436	.685
2.132	2.13	3.650	.644
1.497	1.86	3.847	.572
.862	1.43	3.882	.440
.227	.723	4.033	.227

TABLE 14 - Run 12

$M_0 = 6.287$   $P_0 = 15.15 \text{ atm}$   
 $Re_0 = 6.517$   $T_c = 547 \text{ K}$   
 $\frac{N}{T_0} = 3.864$   $T_0 = 619 \text{ K}$   
 $C_0 = 24.91 \times 10^{-4}$   $U_0 = 990 \text{ m/sec}$

Y (m)	N	T/T <sub>0</sub>	U/U <sub>0</sub>
18.74	6.28	1.000	1.000
18.11	6.24	1.011	1.000
16.84	6.14	1.044	.999
15.57	5.92	1.110	.994
14.30	5.54	1.222	.984
13.03	5.13	1.390	.964
11.76	4.67	1.589	.937
10.49	4.17	1.839	.901
9.218	3.69	2.139	.860
7.948	3.24	2.455	.809
6.678	2.82	2.801	.753
5.408	2.43	3.169	.689
4.138	2.08	3.528	.623
2.868	1.74	3.872	.547
1.598	1.37	4.010	.489
.963	1.38	4.074	.443
.328	.971	4.212	.317
.279	.685	4.397	.215
	.491	4.010	.156

TABLE 13 - Run 11

$M_0 = 6.37$   $P_0 = 15.16 \text{ atm}$   
 $Re_0 = 7.511$   $T_c = 547 \text{ K}$   
 $\frac{N}{T_0} = 3.808$   $T_0 = 60.0 \text{ K}$   
 $C_0 = 17.81 \times 10^{-4}$   $U_0 = 989 \text{ m/sec}$

Y (m)	N	T/T <sub>0</sub>	U/U <sub>0</sub>
22.561	6.37	1.000	1.000
21.311	6.31	1.017	.999
20.041	6.21	1.046	.997
18.771	6.055	1.093	.994
17.501	5.842	1.158	.977
16.231	5.57	1.248	.962
14.961	5.229	1.372	.945
13.691	4.932	1.491	.923
12.421	4.562	1.660	.896
11.151	4.195	1.851	.867
9.881	3.872	2.034	.835
8.611	3.551	2.263	.787
7.341	3.228	2.473	.752
6.071	2.903	2.724	.700
4.801	2.581	2.982	.640
3.531	2.26	3.256	.576
2.261	1.965	3.484	.436
.991	1.493	3.458	.309
.483	1.037	3.593	.279
.279	.571	3.848	.176

TABLE 15 - Run 13

$M_\delta = 6.204$   
 $Re_\delta = 8.156$   
 $\frac{D}{T_\delta} = 3.640$   
 $Cq = 24.52 \times 10^{-4}$   
 $P_0 = 15.15 \text{ atm}$   
 $T_c = 547^\circ K$   
 $T_\delta = 62.9^\circ K$   
 $U_\delta = 987 \text{ m/sec}$

Y (mm)	M	T/T <sub>0</sub>	u/u <sub>0</sub>
26.24	6.20	1.000	1.000
19.89	6.11	1.029	.999
18.62	5.98	1.069	.997
17.15	5.77	1.130	.988
16.08	5.69	1.220	.977
14.81	5.06	1.376	.957
13.54	4.66	1.562	.932
12.27	4.15	1.797	.897
11.63	4.02	1.862	.883
11.00	3.75	2.026	.861
10.36	3.54	2.162	.839
9.728	3.35	2.293	.818
9.093	3.16	2.430	.794
8.458	2.91	2.577	.770
7.823	2.79	2.734	.743
7.188	2.60	2.893	.713
6.553	2.44	3.032	.685
5.918	2.30	3.162	.657
5.283	2.16	3.292	.625
4.648	2.03	3.355	.599
4.013	1.82	3.562	.555
3.378	1.68	3.682	.520
2.763	1.56	3.709	.486
2.108	1.39	3.772	.436
1.473	1.25	3.740	.388
.838	.980	3.734	.305
.279	.516	3.734	.161

TABLE 16 - Run 14

$M_\delta = 6.22$   
 $Re_\delta = 8450$   
 $\frac{D}{T_\delta} = 3.759$   
 $Cq = 24.90 \times 10^{-4}$   
 $P_0 = 15.15 \text{ atm}$   
 $T_c = 547^\circ K$   
 $T_\delta = 62.5^\circ K$   
 $U_\delta = 987 \text{ m/sec}$

Y (mm)	M	T/T <sub>0</sub>	u/u <sub>0</sub>
27.61	6.22	1.000	1.000
26.34	6.21	1.005	1.000
25.07	6.19	1.011	1.000
21.89	6.15	1.064	.998
20.62	5.89	1.105	.995
18.72	5.52	1.225	.982
18.08	5.37	1.279	.975
16.82	5.05	1.398	.956
15.54	4.68	1.555	.938
14.91	4.49	1.642	.926
13.64	4.12	1.836	.898
13.01	3.94	1.944	.883
12.37	3.76	2.080	.867
11.74	3.58	2.177	.849
11.10	3.40	2.310	.831
10.46	3.24	2.426	.812
9.830	3.10	2.536	.793
9.195	2.93	2.674	.770
8.560	2.74	2.845	.744
7.925	2.59	2.990	.719
7.290	2.44	3.112	.693
6.655	2.31	3.226	.668
6.020	2.15	3.387	.637
5.395	2.03	3.501	.610
4.750	1.89	3.637	.579
4.115	1.77	3.741	.550
3.480	1.64	3.853	.518
2.845	1.52	3.945	.486
2.210	1.38	4.041	.440
1.575	1.19	4.132	.388
.840	.977	4.132	.313
.486	.815	3.946	.260
.432	.551	3.965	.176
.279	.443	3.893	.140

TABLE 17 - Run 15

$M_g = 6.22$   
 $Re_g = 10.166$   
 $T_g = 3.663$   
 $C_q = 25.80 \times 10^{-4}$   
 $P_o = 15.22 \text{ atm}$   
 $T_c = 547 \text{ K}$   
 $T_g = 62.5 \text{ K}$   
 $U_g = 987 \text{ m/sec}$

$\gamma$ (cm)	M	$T/T_g$	$U/U_g$
30.23	6.22	1.000	1.000
27.69	6.22	1.002	1.000
25.15	6.11	1.033	1.000
22.61	5.84	1.116	.998
20.07	5.35	1.278	.992
17.53	4.69	1.560	.971
14.99	4.06	1.851	.936
12.45	3.40	2.262	.888
9.906	2.85	2.664	.821
7.366	2.32	3.097	.747
4.826	1.86	3.423	.656
2.286	1.40	3.708	.553
1.016	1.04	3.528	.432
.279	.593	3.512	.313
			.179

TABLE 18 - Run 16

$M_g = 6.52$   
 $Re_g = 1716$   
 $T_g = 4.418$   
 $C_q = 0$   
 $P_o = 15.2 \text{ atm}$   
 $T_c = 548 \text{ K}$   
 $T_g = 57.6 \text{ K}$   
 $U_g = 992 \text{ m/sec}$

$\gamma$ (cm)	M	$T/T_g$	$U/U_g$
16.28	6.52	1.000	1.000
13.74	6.52	1.000	1.000
11.20	6.49	1.000	1.000
9.931	6.48	1.012	1.000
8.661	6.47	1.015	1.000
7.391	6.39	1.040	.999
6.121	6.10	1.097	.994
4.851	5.74	1.250	.984
4.216	5.38	1.386	.971
3.835	5.17	1.470	.942
3.581	4.92	1.593	.932
3.327	4.73	1.687	.942
3.073	4.53	1.792	.931
2.819	4.34	1.913	.920
2.565	4.17	2.023	.909
2.311	4.00	2.141	.896
2.057	3.80	2.298	.883
1.803	3.75	2.326	.877
1.549	3.66	2.397	.869
1.292	3.49	2.535	.853
1.041	3.32	2.667	.833
.787	3.10	2.830	.800
.533	2.69	3.155	.733
.279	2.05	3.714	.606
	1.75	3.576	.507

TABLE 19 - Run 17

$M_0 = 6.32$   
 $R_{E0} = 1993$   
 $\frac{Z_0}{T_0} = 4.171$   
 $C_0 = 0$

$P_0 = 15.2 \text{ atm}$   
 $T_c = 548 \text{ K}$   
 $T_0 = 61.0 \text{ K}$   
 $U_0 = 990 \text{ m/sec}$

$\gamma$ (m)	M	$T/T_0$	$U/U_0$
12.47	6.32	1.000	1.000
9.931	6.28	1.011	1.000
8.661	6.20	1.039	.999
7.391	5.97	1.108	.995
6.121	5.60	1.234	.984
4.851	5.03	1.429	.950
3.581	4.39	1.779	.927
2.946	4.02	2.015	.903
2.545	3.87	2.111	.889
2.311	3.72	2.234	.879
2.057	3.61	2.317	.869
1.803	3.49	2.410	.858
1.549	3.36	2.516	.843
1.295	3.23	2.613	.826
1.041	3.04	2.713	.792
.787	2.76	2.832	.734
.533	2.17	3.221	.616
.279	1.24	4.010	.392

TABLE 20 - Run 18

$M_0 = 6.44$   
 $R_{E0} = 2349$   
 $\frac{Z_0}{T_0} = 4.346$   
 $C_0 = 0$

$P_0 = 15.2 \text{ atm}$   
 $T_c = 547 \text{ K}$   
 $T_0 = 59.0 \text{ K}$   
 $U_0 = 991 \text{ m/sec}$

$\gamma$ (m)	M	$T/T_0$	$U/U_0$
15.29	6.44	1.000	1.000
12.75	6.43	1.002	.999
10.21	6.30	1.042	.999
7.671	5.79	1.206	.989
6.401	5.36	1.366	.974
5.131	4.86	1.583	.950
3.861	4.30	1.889	.918
2.591	3.76	2.261	.878
1.956	3.48	2.490	.834
1.321	3.16	2.763	.815
.686	2.48	3.172	.685
.432	1.78	3.778	.538
.279	1.40	3.988	.435

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TABLE 21 - Run 19

$M_0 = 6.45$	$P_0 = 15.2 \text{ atm}$	$M_0 = 6.68$	$P_0 = 20.05 \text{ atm}$
$Re_0 = 3023$	$T_c = 547 \text{ K}$	$Re_0 = 3296$	$T_c = 550 \text{ K}$
$T_0 = 4.297$	$T_0 = 58.6 \text{ K}$	$T_0 = 4.381$	$T_0 = 55.5 \text{ K}$
$T_0$	$U = 991 \text{ m/sec}$	$T_0$	$U = 998 \text{ m/sec}$
$C_q = 0$		$C_q = 0$	

Y (m)	M	T/T <sub>0</sub>	U/U <sub>0</sub>
27.20	6.45	1.000	1.000
24.66	6.45	1.007	1.000
22.12	6.44	1.004	1.000
19.58	6.41	1.012	.999
17.04	6.38	1.020	.999
14.50	6.34	1.034	.998
13.23	6.28	1.051	.998
11.96	6.18	1.081	.996
10.69	6.03	1.132	.994
9.423	5.81	1.208	.989
8.153	5.47	1.333	.979
6.883	5.04	1.514	.942
5.613	4.58	1.782	.938
4.343	4.13	2.004	.907
3.708	3.91	2.150	.889
3.073	3.65	2.350	.867
2.819	3.56	2.422	.859
2.565	3.54	2.436	.855
2.311	3.37	2.594	.840
2.057	3.26	2.693	.829
1.803	3.14	2.806	.816
1.549	3.04	2.901	.803
1.295	2.91	3.017	.783
1.041	2.71	3.145	.746
.787	2.42	3.313	.681
.533	2.08	3.750	.665
.406	1.54	4.042	.479
.279	1.07	4.459	.349

TABLE 22 - Run 20

$M_0 = 6.68$	$P_0 = 20.05 \text{ atm}$
$Re_0 = 3296$	$T_c = 550 \text{ K}$
$T_0 = 4.381$	$T_0 = 55.5 \text{ K}$
$T_0$	$U = 998 \text{ m/sec}$
$C_q = 0$	

Y (m)	M	T/T <sub>0</sub>	U/U <sub>0</sub>
19.20	6.68	1.000	1.000
12.85	6.65	1.009	1.000
11.58	6.63	1.016	1.000
10.31	6.55	1.039	1.000
9.042	6.48	1.060	.999
8.407	6.37	1.093	.997
7.772	6.24	1.135	.995
7.137	6.06	1.193	.990
6.502	5.84	1.266	.984
5.867	5.60	1.356	.976
5.232	5.32	1.468	.965
4.597	5.05	1.586	.952
3.962	4.77	1.719	.937
3.327	4.46	1.883	.920
2.692	4.19	2.058	.901
2.438	3.90	2.266	.875
2.184	3.77	2.365	.867
1.930	3.64	2.464	.857
1.676	3.50	2.591	.843
1.422	3.39	2.683	.831
1.168	3.25	2.829	.818
.914	3.09	2.970	.798
.787	2.93	3.063	.767
.660	2.80	3.120	.741
.533	2.58	3.289	.701
.406	2.33	3.459	.646
.279	1.93	3.703	.557
	1.45	4.085	.439

TABLE 23 - Run 21

$M_\delta = 6.41$   
 $Re_\delta = 3891$   
 $\frac{T_w}{T_\delta} = 4.116$   
 $C_f = 0$   
 $P_o = 24.95 \text{ atm}$   
 $T_c = 550 \text{ K}$   
 $T_\delta = 60.0 \text{ K}$   
 $U_\delta = 994 \text{ m/sec}$

$Y$ (mm)	$M$	$T/T_\delta$	$U/U_\delta$
21.82	6.41	1.000	1.000
15.47	6.41	1.000	1.000
11.66	6.34	1.019	.999
10.39	6.30	1.032	.998
9.119	6.16	1.076	.998
7.849	5.87	1.171	.991
6.579	5.46	1.317	.977
5.309	4.94	1.530	.954
4.039	4.38	1.812	.920
2.769	3.75	2.223	.873
1.499	3.12	2.749	.808
.864	2.73	3.059	.746
.737	2.60	3.053	.709
.610	2.40	3.259	.675
.483	2.09	3.472	.607
.356	1.65	3.837	.505
.279	1.36	4.032	.427



TABLE 24 SUMMARY OF SKIN FRICTION AND HEAT TRANSFER DATA,  $T_w/T_b = 5.2$ 

$$T_w/T_b = 5.2$$

ROW	X	$M_B$	$P_o$	$Re_x \times 10^{-6}$	$Re_\theta$	$T_w/T_b$	$C_q \times 10^6$	$C_f \times 10^6$	$C_f/C_{fo}$	$2C_q/C_{fo}$	$St \times 10^4$	$\frac{St}{St_o}$
$C_q = 0 \quad T_w/T_b = 5.44$												
22	377.8	6.46	15.22	3.028	1619	5.45	0	15.6			6.77	
23	428.6	6.46	15.25	3.323	1853	5.116	0	11.85	1.000	0	6.42	1.000
24	479.4	6.62	15.08	4.210	2520	5.722	0	14.74	1.000	0	6.69	1.000
25	530.2	6.65	15.12	4.285	2667	5.427	0	12.10	1.000	0	5.18	1.000
$C_q = 8.77 \times 10^{-4} \quad T_w/T_b = 5.45$												
26	377.8	6.45	15.01	3.468	2994	5.210	8.944	10.91	.656	1.076	5.45	.754
27	428.6	6.50	15.15	3.552	3448	5.502	8.932	9.11	.738	1.508	4.66	.726
28	479.4	6.64	15.08	4.438	4554	5.741	8.432	10.83	.735	1.144	4.26	.637
29	530.2	6.55	15.05	4.701	5281	5.348	8.756	7.82	.646	1.439	3.97	.765
$C_q = 17.2 \times 10^{-4} \quad T_w/T_b = 5.07$												
30	377.8	6.21	15.22	2.894	4519	4.752	17.57	6.22	.374	2.114	3.19	.441
31	428.6	6.30	15.15	3.495	5365	4.954	17.14	5.76	.486	2.892	3.28	.511
32	479.4	6.39	15.20	3.885	6223	5.119	17.45	6.75	.458	2.368	2.68	.401
33	530.2	6.62	15.05	5.050	8048	5.468	16.46	8.14	.673	2.721	2.58	.498
$C_q = 24.6 \times 10^{-4} \quad T_w/T_b = 4.85$												
34	377.8	6.27	15.08	3.264	6826	4.800	24.42	6.26	.377	2.938	2.26	.312
35	428.6	6.33	15.12	4.045	8651	4.872	22.96	3.98	.336	3.875	1.85	.288
36	479.4	6.27	15.15	3.940	8969	4.838	26.47	2.58	.184	3.592	1.98	.276
37	530.2	6.37	15.12	4.773	10640	4.887	24.44	5.34	.441	4.040	1.88	--
$C_q = 0 \quad T_w/T_b = 5.58$												
38	377.8	6.53	15.05	3.161	1713	5.582	0	16.62	1.000	0	7.23	1.000

TABLE 25 SUMMARY OF BOUNDARY LAYER PARAMETERS,  $T_w/T_g = 5.2$  $T_w/T_g = 5.2$ 

RUN	X	$Re_x \times 10^{-6}$	$T_w/T_g$	$C_q \times 10^{-4}$	$\theta$	$\delta^*$	$\delta$	$\theta$	$Re_\theta$	$\theta^*$
				$C_q = 0$	$T_w/T_g = 5.44$					
22	377.8	3.028	5.45	0	.202	3.22	5.65	NC	1619	
23	428.6	3.323	5.116	0	.239	3.54	6.70	NC	1853	14.81
24	479.4	4.210	5.722	0	.287	4.77	8.30	.300	2520	16.62
25	530.2	4.285	5.427	0	.330	5.62	9.15	NC	2667	15.21
				$C_q = 8.77 \times 10^{-4}$	$T_w/T_g = 5.45$					
26	377.8	3.468	5.210	8.944	.370	5.25	9.00	.328	2994	14.19
27	428.6	3.552	5.502	8.932	.416	5.94	10.70	NC	3448	14.29
28	479.4	4.438	5.741	8.482	.492	8.04	12.70	.604	4554	16.34
29	530.2	4.701	5.348	8.756	.596	8.58	14.20	1.016	5281	14.33
				$C_q = 17.2 \times 10^{-4}$	$T_w/T_g = 5.07$					
30	377.8	2.894	4.752	17.570	.590	7.42	12.00	.880	4519	12.58
31	428.6	3.495	4.954	17.140	.658	8.65	14.20	NC	5365	13.14
32	479.4	3.885	5.119	17.450	.964	11.06	16.50	1.285	6223	11.47
33	530.2	5.050	5.468	16.460	.845	12.74	19.4	1.620	8048	15.08
				$C_q = 24.6 \times 10^{-4}$	$T_w/T_g = 4.85$					
34	377.8	3.264	4.800	24.420	.790	11.24	16.50	1.28	6826	14.23
35	428.6	4.045	4.872	22.960	.917	14.00	21.00	1.39	8651	15.28
36	479.4	3.948	4.838	26.470	1.090	14.26	19.70	1.86	8969	13.07
37	530.2	4.773	4.887	24.440	1.182	16.56	24.00	2.14	10640	14.01
				$C_q = 0$	$T_w/T_g = 5.58$					
38	377.8	3.141	5.582	0	.206	3.47	5.90	.214	1713	16.85

TABLE 27 - Run 23

$M_0 = 6.46$   $P_0 = 15.25 \text{ atm}$   
 $Re_0 = 1853$   $T_t = 550^\circ K$   
 $T_u/T_0 = 5.116$   $T_0 = 58.8^\circ K$   
 $C_q = 0$   $U_0 = 993 \text{ m/sec}$

Y mm	M	T/T <sub>0</sub>	U/U <sub>0</sub>
10.29	6.46	1.000	1.000
7.747	6.24	1.065	.996
6.477	5.90	1.170	.988
5.207	5.39	1.356	.971
3.937	4.78	1.628	.944
2.667	4.18	1.984	.911
1.397	3.37	2.559	.836
1.143	2.93	2.909	.773
.889	2.34	3.515	.679
.635	1.60	4.459	.522
.508	1.22	4.733	.420
.381	.991	5.093	.346
.330	.941	5.069	.328

TABLE 26 - Run 22

$M_0 = 6.46$   $P_0 = 15.22 \text{ atm}$   
 $Re_0 = 1619$   $T_t = 546^\circ K$   
 $T_u/T_0 = 5.45$   $T_0 = 58.7^\circ K$   
 $C_q = 0$   $U_0 = 992 \text{ m/sec}$

Y mm	M	T/T <sub>0</sub>	U/U <sub>0</sub>
12.66	6.45	1.000	1.000
11.39	6.46	1.000	1.000
10.12	6.44	1.008	1.000
8.217	6.41	1.015	1.000
7.982	6.37	1.027	.999
6.947	6.30	1.051	.999
6.312	6.17	1.087	.996
5.677	5.98	1.147	.991
5.042	5.68	1.249	.983
4.407	5.30	1.399	.971
3.772	4.85	1.610	.953
3.137	4.41	1.869	.933
2.502	4.03	2.131	.910
1.967	3.68	2.420	.885
1.613	3.51	2.552	.869
1.359	3.27	2.722	.834
1.105	2.93	2.940	.778
.851	2.46	3.331	.695
.597	1.84	4.029	.573
.343	1.18	4.843	.403
.165	1.01	4.828	.343

TABLE 28 Run 24

$M_0 = 6.62$   
 $M_{0.9} = 2520$   
 $T_c = 5.722$   
 $T_0 = 56.0^\circ\text{K}$   
 $C_q = 0$   
 $P_c = 15.08 \text{ atm}$   
 $T_c = 546^\circ\text{K}$   
 $T_0 = 56.0^\circ\text{K}$   
 $U_0 = 993 \text{ m/sec}$

Y	M	T/T <sub>0</sub>	U/U <sub>0</sub>
13.27	6.62	1.000	1.000
12.00	6.55	1.021	1.000
10.73	6.43	1.059	1.000
10.10	6.35	1.084	.999
9.462	6.24	1.117	.997
8.827	6.09	1.168	.994
8.192	5.92	1.227	.991
7.557	5.70	1.309	.984
6.922	5.47	1.397	.977
6.287	5.22	1.502	.966
5.652	4.96	1.627	.955
5.017	4.69	1.769	.941
4.382	4.43	1.919	.928
3.747	4.16	2.101	.912
3.112	3.91	2.298	.895
2.478	3.67	2.522	.877
1.843	3.45	2.786	.858
1.208	3.24	3.088	.836
0.573	3.03	3.438	.812
0.000	2.82	3.848	.786
	2.62	4.328	.758
	2.42	4.888	.728
	2.22	5.538	.696
	2.02	6.288	.662
	1.82	7.138	.626
	1.62	8.088	.588
	1.42	9.138	.548
	1.22	10.288	.506
	1.02	11.538	.462
	0.82	12.888	.416
	0.62	14.338	.368
	0.42	15.888	.318
	0.22	17.538	.266
	0.02	19.288	.212

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TABLE 29 - Run 25

$M_0 = 6.45$   
 $M_{0.9} = 2667$   
 $T_c = 5.427$   
 $T_0 = 58.6^\circ\text{K}$   
 $C_q = 0$   
 $P_c = 15.12 \text{ atm}$   
 $T_c = 546^\circ\text{K}$   
 $T_0 = 58.6^\circ\text{K}$   
 $U_0 = 990 \text{ m/sec}$

Y	M	T/T <sub>0</sub>	U/U <sub>0</sub>
15.29	6.45	1.000	1.000
14.02	6.43	1.006	1.000
13.39	6.41	1.010	.998
12.75	6.38	1.020	.999
12.12	6.33	1.036	1.000
11.48	6.28	1.051	.999
10.85	6.20	1.076	.998
10.21	6.10	1.109	.996
9.576	5.98	1.150	.995
8.941	5.84	1.199	.991
8.306	5.66	1.259	.985
7.671	5.46	1.334	.978
7.036	5.25	1.416	.969
6.401	5.21	1.423	.965
5.766	4.79	1.620	.946
5.131	4.55	1.747	.931
4.496	4.31	1.888	.918
3.861	4.06	2.057	.903
3.226	3.80	2.247	.883
2.591	3.54	2.467	.862
1.956	3.29	2.699	.838
1.321	3.19	2.806	.829
0.686	3.06	2.900	.808
0.051	2.96	2.961	.778
	2.59	3.146	.712
	2.20	3.496	.638
	1.89	3.961	.577
	1.56	4.506	.502
	1.38	4.488	.452

TABLE 30 - Run 26

$M_0 = 6.45$   
 $R_{\theta} = 2994$   
 $T_0/T_8 = 5.210$   
 $C_q = 8.94 \times 10^{-4}$   
 $P_0 = 15.01 \text{ atm}$   
 $T_c = 546^\circ\text{K}$   
 $T_8 = 59.2^\circ\text{K}$   
 $U_8 = 995 \text{ m/sec}$

Y	M	T/T <sub>8</sub>	U/U <sub>8</sub>
13.75	6.45	1.000	1.000
12.48	6.44	1.003	1.000
11.21	6.39	1.000	1.000
9.944	6.23	1.047	.999
8.674	5.88	1.152	.988
7.404	5.32	1.353	.970
6.134	4.67	1.644	.937
4.864	4.03	2.010	.895
3.594	3.47	2.449	.851
2.324	3.00	2.892	.800
1.689	2.74	3.167	.760
1.054	2.25	3.517	.659
.419	1.15	4.720	.392
.165	.795	4.814	.273

TABLE 31 - Run 27

$M_0 = 6.50$   
 $R_{\theta} = 3448$   
 $T_0/T_8 = 5.502$   
 $C_q = 8.93 \times 10^{-4}$   
 $P_0 = 15.15 \text{ atm}$   
 $T_c = 548^\circ\text{K}$   
 $T_8 = 58.0^\circ\text{K}$   
 $U_8 = 992 \text{ m/sec}$

Y	M	T/T <sub>8</sub>	U/U <sub>8</sub>
17.56	6.50	1.000	1.000
15.02	6.50	1.000	1.000
12.48	6.49	1.035	1.000
11.21	6.40	1.091	.996
9.940	5.87	1.196	.987
8.672	5.42	1.356	.971
7.402	4.82	1.572	.948
6.132	4.27	1.820	.920
4.862	3.81	2.121	.886
3.592	3.30	2.467	.846
2.322	3.06	2.899	.800
1.687	2.723	3.237	.754
1.052	1.986	3.984	.613
.417	.851	5.371	.303
.165	.673		

TABLE 31 - Run 29

$M_B = 6.55$   
 $P_O = 15.05 \text{ atm}$   
 $R_{Og} = 5281$   
 $T_t = 548^\circ K$   
 $T_B = 57.3^\circ K$   
 $\frac{T_B}{T_t}$   
 $C_q = 8.76 \times 10^{-4}$   
 $U_B = 993 \text{ m/sec}$

Y	M	T/T <sub>B</sub>	U/U <sub>B</sub>
16.31	6.55	1.000	1.000
17.04	6.42	1.036	.999
15.77	6.22	1.098	.996
14.50	5.95	1.185	.990
13.23	5.63	1.298	.980
11.96	5.29	1.437	.969
10.69	4.92	1.601	.952
9.423	4.56	1.786	.931
8.153	4.17	2.021	.905
6.883	3.80	2.268	.875
5.613	3.46	2.540	.843
4.343	3.26	2.712	.821
3.073	3.11	2.861	.803
1.803	2.92	3.094	.780
0.533	2.73	3.279	.755
	2.53	3.525	.725
	2.31	3.771	.686
	2.20	3.898	.660
	2.08	4.021	.639
	1.96	4.103	.616
	1.82	4.174	.593
	1.60	4.282	.521
	1.03	3.084	.355
	.644	2.224	.293
	.614	.583	.149

TABLE 32 - Run 28

$M_B = 6.64$   
 $P_O = 15.08 \text{ atm}$   
 $R_{Og} = 4554$   
 $T_t = 546^\circ K$   
 $T_B = 55.7^\circ K$   
 $\frac{T_B}{T_t}$   
 $C_q = 8.432 \times 10^{-4}$   
 $U_B = 996 \text{ m/sec}$

Y	M	T/T <sub>B</sub>	U/U <sub>B</sub>
19.58	6.64	1.000	1.000
17.04	6.54	1.032	1.000
15.77	6.43	1.068	1.000
14.50	6.24	1.126	.998
13.23	6.01	1.205	.994
11.96	5.70	1.314	.985
10.69	5.30	1.479	.972
9.423	4.89	1.674	.952
8.153	4.46	1.907	.929
6.883	4.05	2.169	.899
6.248	3.81	2.365	.882
5.613	3.62	2.505	.864
4.978	3.42	2.675	.843
4.343	3.24	2.853	.824
4.089	3.14	2.949	.814
3.835	3.08	3.005	.805
3.581	2.99	3.109	.795
3.327	2.91	3.205	.786
3.073	2.84	3.289	.777
2.819	2.78	3.356	.768
2.565	2.70	3.444	.756
2.311	2.59	3.612	.742
2.057	2.50	3.718	.727
1.803	2.43	3.783	.712
1.549	2.30	3.909	.685
1.295	2.13	4.054	.646
1.041	1.92	4.247	.595
.787	1.62	4.573	.522
.533	1.21	5.085	.418
.406	1.02	5.268	.353
.279	.834	5.418	.292

TABLE 34 -- Run 30

$M_B = 6.21$   
 $B_{0H} = 4519$   
 $\frac{B_0}{T_B} = 4.752$   
 $C_q = 17.6 \times 10^{-4}$   
 $P_0 = 15.22 \text{ atm}$   
 $T_c = 547^\circ \text{K}$   
 $T_B = 63.6^\circ \text{K}$   
 $U_B = 993 \text{ m/sec}$

$\frac{Y}{M}$	M	$T/T_B$	$U/U_B$
14.00	6.21	1.000	1.000
12.72	5.97	1.071	.995
11.46	5.63	1.178	.984
10.18	5.11	1.367	.962
9.550	4.79	1.506	.946
8.915	4.50	1.644	.930
8.280	4.24	1.779	.912
7.645	3.97	1.913	.891
7.010	3.73	2.095	.869
6.375	3.48	2.274	.844
5.740	3.25	2.444	.820
5.105	3.03	2.613	.793
4.470	2.83	2.777	.766
3.835	2.62	3.045	.735
3.200	2.44	3.289	.707
2.565	2.24	3.491	.674
1.930	2.01	3.731	.626
1.295	1.66	4.016	.535
1.041	1.42	4.151	.469
.787	1.14	4.469	.390
.533	.802	4.761	.251
.406	.689	4.750	.242
.330	.631	4.744	.221

TABLE 35 Run 31

$M_B = 6.30$   
 $B_{0H} = 5365$   
 $\frac{B_0}{T_B} = 4.954$   
 $C_q = 17.14 \times 10^{-4}$   
 $P_c = 15.15 \text{ atm}$   
 $T_c = 547^\circ \text{K}$   
 $T_B = 61.6^\circ \text{K}$   
 $U_B = 991 \text{ m/sec}$

$\frac{Y}{M}$	M	$T/T_B$	$U/U_B$
17.71	6.30	1.000	1.000
16.99	6.03	1.050	.995
13.92	5.76	1.168	.989
12.65	5.40	1.292	.975
11.36	4.96	1.470	.955
10.11	4.49	1.698	.929
8.839	4.11	1.908	.901
7.569	3.68	2.189	.865
6.299	3.28	2.503	.824
5.029	2.89	2.968	.777
3.759	2.54	3.238	.725
3.124	2.35	3.468	.695
2.489	2.18	3.668	.662
1.854	1.94	3.923	.611
1.219	1.60	4.163	.519
.584	.924	4.778	.321
.330	.673	4.851	.237

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TABLE 37 - Run 33

$M_0 = 6.42$   
 $R_{00} = 804.0$   
 $T_0 = 5.448$   
 $T_0 = 15.05 \text{ atm}$   
 $T_0 = 546.0^\circ\text{K}$   
 $T_0 = 56.0^\circ\text{K}$   
 $C_0 = 16.46 \times 10^{-4}$   
 $U_0 = 993 \text{ m/sec}$

Y	M	T/T <sub>0</sub>	W/W <sub>0</sub>
24.46	6.42	1.000	1.000
22.12	6.41	1.063	.998
19.58	6.04	1.180	.992
17.04	5.45	1.394	.973
14.50	4.72	1.737	.939
11.96	4.03	2.168	.892
9.423	3.37	2.662	.831
6.883	2.76	3.272	.754
4.343	2.22	3.908	.664
3.073	1.97	4.229	.612
2.438	1.81	4.457	.578
1.803	1.67	4.558	.540
1.549	1.53	4.727	.502
1.295	1.43	4.761	.473
1.041	1.29	4.871	.431
.787	1.09	5.054	.370
.660	.991	5.123	.339
.533	.922	5.132	.316
.406	.799	5.213	.276
.279	.612	5.353	.214

TABLE 36 - Run 32

$M_0 = 6.39$   
 $R_{00} = 6223$   
 $T_0 = 5.119$   
 $T_0 = 17.45 \times 10^{-4}$   
 $P_0 = 15.20 \text{ atm}$   
 $T_0 = 546.0^\circ\text{K}$   
 $T_0 = 59.7^\circ\text{K}$   
 $U_0 = 989 \text{ m/sec}$

Y	M	T/T <sub>0</sub>	U/U <sub>0</sub>
24.97	6.39	1.000	1.000
22.43	6.35	1.011	1.000
19.89	6.23	1.051	1.000
18.62	6.09	1.098	.999
17.98	6.00	1.127	.998
17.35	5.89	1.166	.995
16.71	5.73	1.222	.992
16.08	5.58	1.274	.986
15.44	5.36	1.358	.979
14.81	5.19	1.427	.971
14.17	5.04	1.490	.963
13.54	4.86	1.569	.954
12.90	4.69	1.653	.944
12.27	4.47	1.773	.931
11.63	4.28	1.882	.918
11.00	4.09	1.995	.904
10.36	3.91	2.111	.889
9.728	3.72	2.241	.873
9.093	3.55	2.376	.856
8.458	3.38	2.510	.837
7.823	3.21	2.653	.818
7.188	3.05	2.791	.798
6.553	2.90	2.943	.778
5.918	2.74	3.094	.755
5.283	2.59	3.261	.731
4.648	2.44	3.424	.706
4.013	2.27	3.611	.677
3.378	2.13	3.781	.649
2.743	1.99	3.957	.619
2.108	1.85	4.075	.585
1.473	1.63	4.265	.527
.838	1.23	4.539	.411
.511	1.03	4.645	.348



TABLE 39 - Run 35

$M_0 = 6.33$   
 $Re_0 = 8651$   
 $\frac{D_V}{T_0} = 4.872$   
 $C_q = 22.96 \times 10^{-4}$   
 $P_0 = 15.12 \text{ atm}$   
 $T_c = 547^\circ \text{K}$   
 $T_0 = 60.6^\circ \text{K}$   
 $U_0 = 988 \text{ m/sec}$

Y	M	T/T <sub>0</sub>	U/U <sub>0</sub>
25.20	6.13	1.000	1.000
22.65	6.10	1.012	.998
20.11	5.79	1.179	.992
17.57	5.12	1.437	.968
15.03	4.30	1.847	.923
12.49	3.53	2.371	.858
9.947	2.85	2.968	.775
7.407	2.12	3.826	.655
4.867	1.65	4.377	.545
3.597	1.42	4.645	.482
2.327	1.17	4.884	.408
1.692	1.03	4.954	.363
1.057	.792	5.011	.280
.279	.334	4.966	.118

TABLE 38 - Run 34

$M_0 = 6.27$   
 $Re_0 = 6826$   
 $\frac{D_V}{T_0} = 4.800$   
 $C_q = 24.42 \times 10^{-4}$   
 $P_0 = 15.08 \text{ atm}$   
 $T_c = 546^\circ \text{K}$   
 $T_0 = 61.9^\circ \text{K}$   
 $U_0 = 988 \text{ m/sec}$

Y	M	T/T <sub>0</sub>	U/U <sub>0</sub>
23.52	6.27	1.000	1.000
20.98	6.17	1.000	1.000
18.44	6.12	1.044	.998
15.90	5.58	1.223	.984
13.36	4.70	1.591	.946
10.82	3.75	2.149	.877
8.280	2.92	2.838	.785
5.740	2.19	3.635	.665
3.200	1.63	4.300	.539
2.565	1.47	4.510	.498
1.930	1.35	4.591	.463
1.676	1.30	4.597	.446
1.422	1.28	4.546	.435
1.168	1.07	4.757	.373
.914	.932	4.771	.325
.660	.773	4.808	.271
.406	.603	4.806	.211
.279	.428	4.865	.151

TABLE 40 - Run 36

$M_0 = 6.27$   
 $R_{00} = 8969$   
 $\frac{R_0}{T_0} = 4.838$   
 $C_0 = 26.47 \times 10^{-4}$   
 $P_0 = 15.15 \text{ atm}$   
 $T_c = 546^\circ \text{K}$   
 $T_0 = 62.0^\circ \text{K}$   
 $U_0 = 986 \text{ m/sec}$

$\frac{Y}{\infty}$	M	$T/T_0$	$U/U_0$
25.49	6.27	1.000	1.000
22.86	5.94	1.000	1.000
20.32	5.34	1.196	.993
17.76	4.60	1.495	.947
15.24	3.85	1.918	.897
12.70	3.18	2.379	.825
10.16	2.56	2.942	.739
7.620	2.08	3.410	.647
5.080	1.62	3.921	.538
3.210	1.43	4.068	.487
2.540	1.19	4.323	.413
1.905	1.08	4.399	.381
1.270	.876	4.505	.313
1.016	.720	4.562	.259
.762	.515	4.622	.186
.635	.428	4.621	.155
.279	.313	4.472	.111

TABLE 41 - Run 37

$M_0 = 6.37$   
 $R_{00} = 10640$   
 $\frac{R_0}{T_0} = 4.887$   
 $C_0 = 24.64 \times 10^{-4}$   
 $P_0 = 15.12 \text{ atm}$   
 $T_c = 547^\circ \text{K}$   
 $T_0 = 60.0^\circ \text{K}$   
 $U_0 = 990 \text{ m/sec}$

$\frac{Y}{\infty}$	M	$T/T_0$	$U/U_0$
32.31	6.37	1.000	1.000
29.77	6.32	1.016	.999
27.23	6.16	1.062	.996
24.69	5.86	1.151	.991
22.15	5.37	1.339	.974
19.61	4.69	1.642	.942
17.07	4.08	1.978	.899
14.53	3.30	2.367	.846
11.99	2.90	2.895	.775
9.449	2.45	3.340	.702
6.909	2.00	3.830	.615
4.369	1.61	4.277	.522
3.099	1.41	4.489	.468
2.444	1.25	4.682	.423
1.829	1.18	4.667	.398
1.575	1.14	4.647	.385
1.321	.979	4.829	.316
1.067	.904	4.839	.312
.813	.803	4.851	.278
.559	.598	4.942	.209
.432	.554	4.904	.182
.305	.476	4.883	.165
.279			

TABLE 42 - Run 38

$M_\infty = 6.53$   
 $Re_\theta = 1713$   
 $T_w = 5.582$   
 $C_q = 0$   
 $P_o = 15.05 \text{ atm}$   
 $T_t = 546^\circ K$   
 $T_\delta = 57.3^\circ K$   
 $U_\delta = 991 \text{ m/sec}$

Y (mm)	M	$T/T_\delta$	$U/U_\delta$
19.36	6.53	1.000	1.000
18.09	6.53	1.000	1.000
16.82	6.53	1.000	1.000
15.54	6.53	1.000	1.000
14.28	6.54	.998	1.000
13.00	6.54	.998	1.000
11.74	6.54	1.000	1.000
10.46	6.53	1.004	1.001
9.195	6.50	1.013	1.002
7.925	6.41	1.041	1.001
6.655	6.19	1.110	.998
5.385	5.73	1.261	.986
4.750	5.43	1.379	.976
4.115	4.97	1.586	.959
3.480	4.52	1.839	.936
2.845	4.09	2.126	.914
2.210	3.71	2.474	.889
1.575	3.34	2.781	.853
1.321	3.16	2.891	.824
1.067	2.94	3.001	.779
.813	2.63	3.206	.720
.559	2.08	3.766	.618
.432	1.66	4.337	.528
.305	1.24	4.886	.419
.279	1.01	5.240	.355

TABLE 43 SUMMARY OF SKIN FRICTION AND HEAT TRANSFER DATA,  $T_w/T_s = 7.6$ 

$T_w/T_s = 7.6$													
RUN	X mm	$M_s$	$P_o$ atm	$Re_x \times 10^{-6}$	$Re_\theta$	$T_w/T_s$	$C_q$	$T_w/T_s$	$C_f \times 10^4$	$C_f/C_{fo}$	$2C_q/C_{fo}$	$St \times 10^4$	$\frac{St}{St_o}$
$C_q = 0 \quad T_w/T_s = 7.87$													
39	277.3	6.31	15.12	2.840	1223	7.614	0	19.54	1.000	0	28.2	1.000	
40	428.6	6.45	15.05	3.429	1720	7.780	0	17.70	1.000	0	29.4	1.000	
41	479.4	6.61	15.12	4.252	2200	8.080	0	15.74	1.000	0	23.3	1.000	
42	530.2	6.62	15.08	4.803	2844	8.018	0	14.50	1.000	0	20.6	1.000	
$C_q = 8.68 \times 10^{-4} \quad T_w/T_s = 7.65$													
43	479.4	6.51	15.08	4.099	4541	7.650	8.68	11.20	.712	1.103	10.71	.440	
$C_q = 16.2 \times 10^{-4} \quad T_w/T_s = 7.65$													
44	479.4	6.57	15.08	4.514	6365	7.649	16.17	8.41	.534	2.055	5.18	.222	
$C_q = 24.4 \times 10^{-4} \quad T_w/T_s = 7.26$													
45	479.4	6.49	15.01	4.632	8928	7.259	24.42	6.06	.385	3.103	2.82	.121	
$C_q = 0 \quad T_w/T_s = 7.81$													
46	479.4	6.43	20.01	4.897	2360	7.805	0	14.56	1.000	0	23.08	1.000	

TABLE 44 SUMMARY OF BOUNDARY LAYER PARAMETERS,  $T_w/T_\infty = 7.6$   
 $T_w/T_\infty = 7.6$

RUN	X	Pe $\times 10^{-6}$	$T_w/T_\infty$	$C_q \times 10^4$	$\theta$	$\theta^*$	$\theta$	Re $\theta$	$\theta^*$
					mm	mm	mm		
				$C_q = 0$		$T_w/T_\infty = 7.87$			
39	477.2	2.840	7.614	0	.176	3.78	6.2	132.7	21.48
40	472.7	3.429	7.780	0	.215	4.72	7.5	172.0	21.95
41	479.4	4.252	8.080	0	.248	5.56	8.5	220.0	22.42
42	510.2	4.803	8.012	0	.314	6.57	10.2	286.4	20.92
				$C_q = 8.6 \times 10^{-4}$		$T_w/T_\infty = 7.65$			
43	479.4	4.099	7.650	2.68	.531	8.45	15.0	454.1	15.91
				$C_q = 16.2 \times 10^{-4}$		$T_w/T_\infty = 7.65$			
44	479.4	4.514	7.649	16.17	.676	12.90	17.5	536.6	19.02
				$C_q = 24.4 \times 10^{-4}$		$T_w/T_\infty = 7.26$			
45	479.4	4.632	7.259	24.42	.924	17.42	23.0	892.8	12.35
				$C_q = 0$		$T_w/T_\infty = 7.81$			
46	479.4	4.297	7.805	0	.280	5.24	8.7	226.0	12.72

TABLE 45 - Run 39

$M = 6.31$   
 $P_0 = 15.12 \text{ atm}$   
 $P_{0g} = 1323$   
 $T_c = 549^\circ\text{K}$   
 $T_g = 7.614$   
 $T_g = 61.3^\circ\text{K}$   
 $C_q = 0$   
 $U_g = 991. \text{ m/sec}$

$Y$ (mm)	$M$	$T/T_g$	$U/U_g$
24.10	6.29	1.000	1.000
17.76	6.34	1.000	1.000
13.94	6.34	1.000	1.000
11.41	6.34	1.000	1.000
10.14	6.31	1.000	1.000
8.865	6.25	1.021	1.000
7.595	6.07	1.077	.998
6.325	5.75	1.191	.993
5.035	5.18	1.423	.978
4.420	4.83	1.600	.967
3.785	4.41	1.867	.950
2.515	3.66	2.452	.909
1.880	3.33	2.809	.886
1.499	3.05	3.143	.856
1.245	2.79	3.496	.826
.991	2.42	4.037	.771
.737	1.89	4.967	.668
.610	1.60	5.555	.596
.483	1.32	6.081	.515
.279	.827	6.942	.345

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TABLE 46 - Run 40

$M = 6.45$   
 $P_0 = 15.05 \text{ atm}$   
 $Re = 1720$   
 $T_c = 550^\circ\text{K}$   
 $T_g = 7.780$   
 $T_g = 59.2^\circ\text{K}$   
 $C_q = 0$   
 $U = 995 \text{ m/sec}$

$Y$ (mm)	$M$	$T/T$	$U/U$
12.89	6.45	1.000	1.000
12.26	6.44	1.005	1.000
11.62	6.42	1.011	1.000
10.99	6.38	1.025	1.000
10.35	6.33	1.042	1.000
9.716	6.25	1.068	1.000
9.081	6.14	1.103	.999
8.446	5.98	1.156	.997
7.811	5.80	1.222	.994
7.176	5.58	1.308	.988
6.541	5.32	1.418	.981
5.906	5.04	1.551	.972
5.271	4.74	1.709	.961
4.636	4.44	1.892	.947
4.001	4.18	2.079	.933
3.366	3.90	2.307	.918
2.731	3.61	2.592	.900
2.096	3.32	2.911	.879
1.461	2.93	3.412	.849
1.207	2.66	3.807	.803
.953	2.28	4.398	.740
.699	1.71	5.457	.619
.572	1.42	6.036	.542
.445	1.21	6.462	.475
.318	.961	6.905	.391
.279	.761	7.285	.318

TABLE 47 - Run 41

$M_0 = 6.61$   
 $Re_0 = 2200$   
 $T_u/T = 8.080$   
 $C_q = 0$   
 $P_0 = 15.12 \text{ atm}$   
 $T_t = 548^\circ K$   
 $T = 56.4^\circ K$   
 $U = 995 \text{ m/sec}$

Y (mm)	M	T/T	U/U
19.41	6.61	1.000	1.000
18.14	6.61	1.000	1.000
16.74	6.61	1.000	1.000
14.33	6.58	1.010	1.000
11.79	6.42	1.062	1.000
10.52	6.24	1.119	.999
9.246	5.95	1.221	.995
7.976	5.55	1.378	.985
6.706	5.06	1.601	.969
5.436	4.57	1.883	.948
4.166	4.06	2.244	.921
2.896	3.57	2.720	.891
2.261	3.29	3.048	.869
1.626	2.92	3.551	.833
1.372	2.71	3.843	.803
1.118	2.38	4.392	.754
.864	1.91	5.259	.663
.737	1.66	5.775	.604
.610	1.38	6.395	.527
.483	1.09	7.007	.436
.356	.972	7.307	.398
.279	.774	7.512	.321

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TABLE 48 - Run 42

$M_0 = 6.62$   
 $Re_0 = 2844$   
 $T_u/T = 8.018$   
 $C_q = 0$   
 $P_0 = 15.08 \text{ atm}$   
 $T_t = 548^\circ K$   
 $T_g = 56.2^\circ K$   
 $U_g = 995 \text{ m/sec}$

Y (mm)	M	T/T <sub>0</sub>	U/U <sub>0</sub>
23.90	6.62	1.000	1.000
17.55	6.53	1.024	.999
13.74	6.36	1.077	.998
12.47	6.24	1.119	.996
11.20	6.03	1.191	.995
9.931	5.75	1.298	.989
8.661	5.39	1.449	.980
7.391	4.98	1.647	.966
6.121	4.55	1.891	.944
4.851	4.11	2.196	.921
4.216	3.91	2.369	.908
3.581	3.67	2.590	.892
2.946	3.43	2.843	.874
2.311	3.19	3.136	.854
1.676	2.85	3.631	.820
1.041	2.20	4.686	.721
.787	1.71	5.662	.615
.660	1.46	6.187	.548
.533	1.09	7.002	.436
.406	.975	7.151	.394
.279	.763	7.488	.315

TABLE 50 - Run 44

$P_0 = 6.37$   
 $P_0 = 15.08 \text{ atm}$   
 $R_{00} = 6365$   
 $T_c = 549^\circ \text{K}$   
 $T_0 = 7.649$   
 $T_0 = 57.0^\circ \text{K}$   
 $C_1 = 16.17 \times 10^{-4}$   
 $U_0 = 994 \text{ m/sec}$

Y (mm)	H	T/T <sub>0</sub>	U/U <sub>0</sub>
27.94	6.57	1.000	1.000
25.40	6.53	1.012	1.000
22.86	6.44	1.040	1.000
20.32	6.19	1.127	1.000
17.78	5.68	1.315	.991
16.51	5.32	1.465	.980
15.24	4.94	1.618	.957
13.70	4.17	2.116	.923
12.43	3.80	2.409	.896
11.16	3.42	2.761	.864
8.890	3.08	3.129	.829
7.620	2.81	3.454	.795
6.350	2.53	3.846	.754
5.080	2.25	4.267	.708
3.810	1.94	4.824	.649
2.540	1.64	5.411	.580
1.305	1.46	5.767	.534
1.170	1.16	6.359	.444
1.016	1.00	6.384	.407
.745	.903	6.787	.359
.506	.635	7.187	.275
.381	.548	7.317	.234
.279	.428	7.485	.176

TABLE 49 - Run 43

$P_0 = 6.51$   
 $P_0 = 15.08 \text{ atm}$   
 $R_{00} = 4541$   
 $T_c = 551^\circ \text{K}$   
 $T_0 = 7.650$   
 $T_0 = 58.4^\circ \text{K}$   
 $C_1 = 8.68 \times 10^{-4}$   
 $U_0 = 1007 \text{ m/sec}$

Y (mm)	H	T/T <sub>0</sub>	U/U <sub>0</sub>
25.42	6.62	1.000	1.000
22.88	6.63	1.000	1.000
20.34	6.62	1.000	1.000
17.81	6.57	1.000	1.000
15.26	6.20	1.098	.990
12.72	5.58	1.322	.977
11.46	5.18	1.494	.964
10.18	4.78	1.696	.947
8.915	4.38	1.937	.927
7.645	3.98	2.214	.901
6.375	3.60	2.534	.872
5.105	3.22	2.915	.838
4.470	3.05	3.111	.820
3.835	2.87	3.337	.789
3.200	2.68	3.614	.775
2.565	2.48	3.951	.745
1.930	2.18	4.430	.700
1.295	1.79	5.156	.618
.860	1.11	6.511	.430
.533	.950	6.797	.377
.408	.748	7.140	.304
.279	.628	7.280	.258



TABLE 51 - Run 45

$M_0 = 6.49$   
 $R_{\theta} = 0928$   
 $T_c = 7.259$   
 $T_B = 56.2^\circ\text{K}$   
 $C_q = 24.42 \times 10^{-4}$   
 $P_0 = 15.01 \text{ atm}$   
 $T_c = 54.0^\circ\text{K}$   
 $T_B = 56.2^\circ\text{K}$   
 $U_B = 992 \text{ m/sec}$

$\gamma$ (mm)	M	$x/T_B$	$U/U_B$
35.54	6.49	1.000	1.000
33.00	6.49	1.000	1.000
30.46	6.45	1.010	.999
27.92	6.35	1.041	.999
25.38	6.12	1.119	.998
22.84	5.58	1.315	.987
20.30	4.92	1.618	.964
17.76	4.14	2.087	.921
15.22	3.41	2.697	.862
12.68	2.83	3.332	.795
10.14	2.37	3.933	.724
7.595	1.92	4.633	.637
5.055	1.43	5.519	.519
3.785	1.34	5.656	.489
2.515	1.11	6.072	.421
1.800	.963	6.331	.376
1.245	.796	6.612	.316
.991	.632	6.881	.256
.483	.520	7.016	.212
.279	.329	7.216	.136

TABLE 52 - Run 46

$M_0 = 6.43$   
 $R_{\theta} = 2860$   
 $T_c = 54.8^\circ\text{K}$   
 $T_B = 59.1^\circ\text{K}$   
 $C_q = 0$   
 $P_0 = 20.01 \text{ atm}$   
 $T_c = 54.8^\circ\text{K}$   
 $T_B = 59.1^\circ\text{K}$   
 $U_B = 992 \text{ m/sec}$

$\gamma$ (mm)	M	$x/T_B$	$U/U_B$
23.39	6.42	1.000	1.000
17.04	6.43	1.000	1.000
15.77	6.43	1.000	1.000
13.23	6.30	1.009	.999
11.96	6.24	1.030	.999
10.49	6.14	1.073	.997
9.423	5.93	1.156	.995
8.153	5.59	1.288	.986
6.883	5.14	1.481	.971
5.613	4.66	1.727	.951
4.343	4.16	2.043	.923
3.073	3.63	2.477	.889
1.803	3.04	3.159	.841
1.168	2.62	3.784	.792
1.041	2.49	3.993	.772
.916	2.30	4.290	.742
.787	2.06	4.725	.695
.660	1.76	5.310	.629
.533	1.40	6.045	.536
.406	1.09	6.877	.439
.279	.868	7.061	.358

TABLE 53 SUMMARY OF SKIN FRICTION AND HEAT TRANSFER DATA,  $T_w/T_\infty = 7.6$  $\tau_w/\tau_\infty = 7.6$ 

RUN	X mm	H <sub>0</sub>	P <sub>0</sub> atm	Re <sub>x</sub> 10 <sup>-6</sup>	Re <sub>θ</sub>	$T_w/T_\infty$	$c_{fx}10^4$	$c_{fθ}10^4$	cg/cg <sub>0</sub>	2C <sub>q</sub> /C <sub>q0</sub>	St10 <sup>4</sup>	$\frac{SE}{SC}$
47	530.2	6.34	38.07	9.70	4897	7.06	0	9.92	1.000	0	8.3	1.000
48	530.2	6.46	38.07	10.76	6824	7.19	3.70	8.35	.861	.766	5.83	.702
49	530.2	6.47	38.07	10.84	8753	7.01	7.25	7.6	.767	1.464	4.49	.541
50	530.2	6.52	38.07	11.03	11737	6.87	10.13	6.25	.630	2.040	3.64	.439

TABLE 54. SUMMARY OF BOUNDARY LAYER PARAMETERS,  $T_u/T_8 = 7.6$

$T_u/T_8 = 7.6$

RUN	X	$R_{\theta} \times 10^{-6}$	$T_u/T_8$	$c_q \times 10^4$	$\theta$	$\beta^*$	$\delta$	$\delta^*$	Re $\theta$	$\beta^*_{\theta}$
47	530.2	9.70	7.06	0	.265	4.66	8.0	.150	4897	17.6
48	530.2	10.76	7.19	3.70	.336	6.26	9.5	.640	6824	16.91
49	532.0	10.84	7.01	7.25	.428	7.80	11.0	1.36	8753	18.22
50	530.2	11.03	6.87	10.13	.564	9.80	14.2	2.74	11737	17.38

TABLE 56 - Run 48

$N = 6.46$   
 $Re = 6824$   
 $\frac{T_w}{T} = 7.19$   
 $C_q = 3.70 \times 10^{-4}$   
 $P = 38.07 \text{ atm}$   
 $T_t = 508 \text{ K}$   
 $T = 58.7 \text{ K}$   
 $U = 992 \text{ m/sec}$

Y (mm)	M	T/T	U/U
26.25	6.46	1.000	1.000
23.71	6.45	1.003	1.000
21.17	6.43	1.007	1.000
18.63	6.42	1.010	1.000
16.09	6.42	1.014	1.000
13.55	6.40	1.034	1.000
11.01	6.41	1.112	1.000
10.38	5.98	1.162	.998
9.741	5.80	1.226	.994
9.106	5.58	1.305	.988
8.471	5.34	1.402	.980
7.836	5.07	1.521	.969
7.201	4.81	1.649	.957
6.566	4.55	1.797	.944
5.931	4.25	1.978	.926
5.296	3.97	2.176	.908
4.661	3.68	2.409	.885
4.026	3.35	2.716	.856
3.391	3.08	3.015	.827
2.756	2.85	3.285	.800
2.121	2.62	3.600	.770
1.486	2.34	4.070	.730
.851	1.84	4.951	.634
.597	1.51	5.436	.549
.470	1.31	5.848	.492
.343	1.04	6.302	.406
.292	.959	6.641	.377
.191	.911	6.410	.357

TABLE 55 - Run 47

$M = 6.34$   
 $Re = 4897$   
 $T_w/T = 7.06$   
 $C_q = 0$   
 $P_0 = 33.07 \text{ atm}$   
 $T_t = 550^\circ K$   
 $T = 61.0^\circ K$   
 $U = 992.0 \text{ m/sec}$

Y (mm)	M	T/T	U/U
21.22	6.34	1.000	1.000
18.68	6.33	1.003	1.000
16.14	6.32	1.006	1.000
13.60	6.32	1.025	.999
11.06	6.25	1.054	.999
9.792	6.17	1.123	.997
8.522	5.96	1.242	.988
7.252	5.57	1.371	.980
6.617	5.30	1.497	.968
5.932	5.01	1.610	.939
4.712	4.42	1.999	.920
4.077	4.12	2.240	.898
3.442	3.80	2.486	.875
2.807	3.52	2.777	.850
2.172	3.23	3.131	.822
1.537	2.94	4.028	.742
.648	1.94	4.660	.662
.521	1.70	5.066	.603
.394	1.38	5.607	.517
.267	1.08	6.114	.421
.191	1.04	6.103	.403

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TABLE 57 - Run 49

$M = 6.47$	$P = 38.77 \text{ atm}$	$M = 6.52$	$P = 38.77 \text{ atm}$
$T_0 = 8753$	$T_c = 549 \text{ K}$	$R_0 = 11.737$	$T_c = 553 \text{ K}$
$T_0 = 7.01$	$T = 58.6 \text{ K}$	$T_0 = 6.87$	$T = 58.2 \text{ K}$
$C_q = 7.25 \times 10^{-6}$	$U = 993 \text{ m/sec}$	$C_q = 1.013 \times 10^{-6}$	$U = 997 \text{ m/sec}$

Y (mm)	M	T/T	U/U
28.79	6.47	1.000	1.000
26.25	6.46	1.003	1.000
23.71	6.45	1.008	1.000
21.17	6.44	1.010	1.000
18.63	6.44	1.032	1.002
16.09	6.38	1.095	1.003
13.55	6.20	1.167	.999
12.28	5.94	1.335	.989
11.01	5.54	1.620	.979
9.74	5.28	1.938	.970
8.41	5.06	1.679	.957
7.07	4.78	1.799	.945
5.71	4.56	2.117	.913
4.33	4.06	2.507	.873
2.99	3.57	2.981	.826
1.66	3.10	3.688	.771
3.91	2.67	3.780	.740
2.46	2.46	4.122	.706
2.12	2.25	4.559	.669
1.86	2.00	5.236	.649
.851	1.37	5.369	.502
.597	1.37	6.309	.364
.443	.943	6.389	.317
.287	.863	6.482	.270
.191	.768		

TABLE 58 - Run 50

$M = 6.52$	$P = 38.77 \text{ atm}$	$M = 6.52$	$P = 38.77 \text{ atm}$
$R_0 = 11.737$	$T_c = 553 \text{ K}$	$R_0 = 11.737$	$T_c = 553 \text{ K}$
$T_0 = 6.87$	$T = 58.2 \text{ K}$	$T_0 = 6.87$	$T = 58.2 \text{ K}$
$C_q = 1.013 \times 10^{-6}$	$U = 997 \text{ m/sec}$	$C_q = 1.013 \times 10^{-6}$	$U = 997 \text{ m/sec}$

Y (mm)	M	T/T	U/U
28.77	6.52	1.000	1.000
23.69	6.49	1.009	1.000
18.61	6.43	1.031	1.000
16.07	6.24	1.090	.999
13.53	5.64	1.299	.985
12.26	5.16	1.639	.977
10.99	4.69	1.741	.948
9.716	4.22	2.015	.920
8.446	3.84	2.289	.892
7.176	3.27	2.818	.843
5.906	2.89	3.234	.797
4.636	2.52	3.676	.741
3.366	2.17	4.193	.682
2.731	2.01	4.459	.652
2.096	1.83	4.786	.615
1.461	1.62	5.186	.566
.826	1.34	5.617	.488
.572	1.15	5.907	.428
.445	.966	6.181	.368
.318	.832	6.337	.317
.191	.693	6.457	.270

TABLE 59 SUMMARY OF SKIN FRICTION AND HEAT TRANSFER DATA,  $T_w/T_s = 4.1$  $T_w/T_s = 4.1$ 

RUN	X mm	M <sub>s</sub>	P <sub>o</sub>	Re <sub>x</sub> 10 <sup>-6</sup>	Re	T <sub>w</sub> /T <sub>s</sub>	C <sub>q</sub> 10 <sup>4</sup>	C <sub>f</sub> 10 <sup>4</sup>	C <sub>f</sub> /C <sub>f0</sub>	2C <sub>q</sub> /C <sub>f0</sub>	St10 <sup>4</sup>	$\frac{St}{St_0}$
$C_q = 0$ $T_w/T_s = 4.70$												
51	428.6	6.50	38.07	8.529	3841	4.665	0	6.26	1.000	0	4.61	1.000
52	479.4	6.49	38.07	9.260	4557	4.735	0	6.97	1.000	0	4.47	1.000
53	530.2	6.37	38.01	10.13	5997	4.700	0	6.81	1.000	0	4.00	1.000
$C_q = 0$ $T_w/T_s = 4.32$												
54	530.2	6.34	35.01	8.98	5218	4.32	0	7.73	1.000	0	4.64	1.000
$C_q = 4.12 \times 10^{-4}$ $T_w/T_s = 4.41$												
55	530.2	6.50	35.01	9.57	7816	4.41	4.12	6.41	.83	1.066	2.95	.636
$C_q = 8.17 \times 10^{-4}$ $T_w/T_s = 4.37$												
56	530.2	6.45	35.01	9.41	10011	4.37	8.17	5.30	.686	2.114	2.44	.525
$C_q = 12.1 \times 10^{-4}$ $T_w/T_s = 4.35$												
57	530.2	6.47	35.01	9.89	12775	4.35	12.1	4.23	.547	3.123	2.14	.461

TABLE 60 SUMMARY OF BOUNDARY LAYER PARAMETERS,  $T_w/T_g = 4.1$  $T_w/T_g = 4.1$ 

RUN	X	$R_{e_x} \times 10$	$T_w/T_g$	$C_q \times 10^{-4}$	$\theta$	$\delta^*$	$\delta$	$\theta$	Re $\theta$	$\frac{\delta}{\theta}$
$T_w/T_g = 4.32$										
51	428.6	8.529	4.665	0	.193	2.78	5.20	.248	3841	14.40
52	479.4	9.26	4.735	0	.236	3.51	5.85	.284	4557	14.88
53	530.2	10.13	4.700	0	.313	4.70	7.70	.408	5997	15.01
$T_w/T_g = 4.32$										
54	530.2	8.98	4.32	0	.308	4.63	7.8		5218	15.02
$T_w/T_g = 4.41$										
55	530.2	9.57	4.41	4.12	.433	6.52	10.7		7816	15.06
$T_w/T_g = 4.37$										
56	530.2	9.41	4.37	8.17	.564	7.64			10011	13.55
$T_w/T_g = 4.35$										
57	530.2	9.89	4.35	12.1	.685	9.22	14.8		12775	13.46

TABLE 61 - Run 51

$M = 6.50$   
 $Re = 3861$   
 $T_w/T = 4.665$   
 $C_q = 0$   
 $P = 38.07 \text{ atm}$   
 $T_t = 550 \text{ K}$   
 $T = 58.1 \text{ K}$   
 $U = 996 \text{ m/sec}$

Y (mm)	M	T/T	U/U
10.77	6.50	1.000	1.000
9.499	6.50	1.002	1.000
8.864	6.49	1.004	1.000
8.229	6.49	1.005	1.000
7.584	6.47	1.009	.999
6.959	6.43	1.020	.998
6.324	6.34	1.044	.996
5.689	6.21	1.085	.994
5.054	5.94	1.176	.991
4.419	5.66	1.276	.983
3.784	5.21	1.464	.969
3.149	4.72	1.695	.944
2.631	4.29	1.945	.920
2.133	3.89	2.221	.891
1.879	3.69	2.377	.875
1.625	3.51	2.539	.858
1.371	3.33	2.705	.841
1.117	3.14	2.875	.819
.863	2.95	3.063	.793
.736	2.82	3.159	.771
.609	2.53	3.495	.726
.482	2.06	4.040	.635
.431	1.85	4.296	.589
.406	1.78	4.339	.553
.304	1.74	4.128	.542

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TABLE 62 - Run 52

$M = 6.49$   
 $Re = 4557$   
 $T_w/T = 4.735$   
 $C_q = 0$   
 $P_o = 38.07 \text{ atm}$   
 $T_t = 550^\circ K$   
 $T = 58.6^\circ K$   
 $U = 996 \text{ m/sec}$

Y (mm)	M	T/T	U/U
23.62	6.49	1.000	1.000
21.08	6.49	1.000	1.000
18.54	6.48	1.003	1.000
16.00	6.48	1.002	.999
13.46	6.48	1.002	.999
10.92	6.47	1.005	.999
9.650	6.45	1.013	1.000
8.380	6.40	1.027	1.000
7.745	6.35	1.042	.999
7.110	6.26	1.071	.997
6.475	6.09	1.124	.994
5.840	5.86	1.199	.989
5.205	5.56	1.307	.979
4.570	5.18	1.462	.965
3.935	4.78	1.638	.943
3.554	4.52	1.778	.929
3.300	4.38	1.856	.918
2.919	4.14	1.997	.901
2.665	4.01	2.082	.891
2.284	3.76	2.258	.871
2.030	3.58	2.399	.855
1.776	3.64	2.321	.855
1.552	3.25	2.707	.823
1.268	3.09	2.882	.807
1.014	2.93	3.047	.787
.760	2.74	3.194	.753
.557	2.37	3.496	.682
.532	2.30	3.570	.669
.506	2.24	3.656	.652
.430	1.90	4.037	.588
.379	1.72	4.232	.546



TABLE 63 - Run 53

$M = 6.37$   
 $P_o = 38.01 \text{ atm}$   
 $Re = 5997$   
 $T_t = 549^\circ K$   
 $T = 60.2^\circ K$   
 $\frac{T_w}{T} = 4.700$   
 $U = 991 \text{ m/sec}$   
 $C_q = 0$

Y (mm)	M	T/T	U/U
24.75	6.37	1.000	1.000
24.21	6.36	1.002	.999
21.67	6.34	1.008	.999
19.13	6.33	1.012	.998
16.59	6.31	1.018	.998
14.05	6.30	1.021	.998
11.51	6.24	1.038	.998
10.24	6.21	1.052	.999
8.972	6.11	1.083	.998
7.702	5.83	1.174	.990
6.432	5.34	1.348	.973
5.162	4.74	1.609	.943
3.892	4.12	1.951	.902
3.257	3.79	2.174	.876
2.622	3.44	2.442	.843
1.987	3.13	2.722	.810
1.352	2.79	3.076	.769
1.098	2.65	3.224	.747
.844	2.52	3.330	.720
.590	2.21	3.610	.660
.463	1.90	3.953	.594
.336	1.45	4.924	.484

TABLE 64 - Run 54

$M = 6.34$   
 $P_o = 35.01 \text{ atm}$   
 $Re = 5218$   
 $T_t = 548.5^\circ K$   
 $T = 60.7^\circ K$   
 $\frac{T_w}{T} = 4.32$   
 $U = 990 \text{ m/sec}$   
 $C_q = 0$

Y (mm)	M	T/T	U/U
29.74	6.34	1.000	1.000
27.20	6.34	1.000	1.000
24.66	6.34	1.000	1.000
22.12	6.33	1.003	1.000
19.58	6.33	1.005	1.000
17.04	6.31	1.011	1.000
14.50	6.31	1.011	1.000
11.96	6.25	1.030	1.000
10.69	6.20	1.044	.999
9.423	6.12	1.070	.998
8.153	5.89	1.148	.995
6.883	5.45	1.30	.981
6.248	5.20	1.42	.977
5.613	4.92	1.52	.958
4.978	4.62	1.67	.942
4.343	4.31	1.84	.922
3.708	4.02	2.01	.899
3.073	3.70	2.23	.872
2.438	3.38	2.48	.841
1.803	3.06	2.78	.804
1.549	2.92	2.91	.786
1.295	2.79	3.06	.769
1.041	2.65	3.20	.747
.787	2.51	3.29	.718
.660	2.38	3.37	.688
.533	2.17	3.50	.641
.406	1.80	3.88	.558
.279	1.27	4.42	.422

TABLE 65 - Run 55

$M = 6.50$   
 $Re = 7816$   
 $\frac{T_w}{T} = 4.41$   
 $C_q = 4.12 \times 10^{-4}$   
 $P_o = 35.01 \text{ atm}$   
 $T_c = 549.5^\circ K$   
 $T = 58.0^\circ K$   
 $U = 994 \text{ m/sec}$

Y (mm)	M	T/T	U/U
29.84	6.50	1.000	1.000
27.31	6.51	1.000	1.000
24.76	6.48	1.007	1.000
22.22	6.45	1.016	1.000
19.58	6.44	1.021	1.000
17.14	6.44	1.021	1.000
14.61	6.40	1.032	1.000
12.06	6.21	1.092	.997
10.80	6.00	1.160	.994
9.525	5.62	1.30	.983
8.255	5.15	1.49	.965
6.985	4.65	1.73	.940
5.715	4.13	2.03	.904
4.445	3.60	2.40	.858
3.810	3.34	2.62	.830
3.175	3.09	2.83	.799
2.540	2.82	3.10	.764
1.905	2.58	3.36	.726
1.651	2.45	3.51	.705
1.397	2.37	3.58	.691
1.143	2.26	3.72	.670
.889	2.11	3.86	.636
.762	2.01	3.90	.610
.635	1.84	4.00	.567
.508	1.58	4.17	.496
.279	1.14	4.30	.363

TABLE 66 - Run 56

$M = 6.45$   
 $Re = 10,011$   
 $\frac{T_w}{T} = 4.38$   
 $C_q = 8.17 \times 10^{-4}$   
 $P_o = 35.01 \text{ atm}$   
 $T_c = 548.5^\circ K$   
 $T = 59.2^\circ K$   
 $U = 995.0 \text{ m/sec}$

Y (mm)	M	T/T	U/U
29.74	6.45	1.000	1.000
27.20	6.44	1.004	1.000
24.66	6.43	1.005	1.000
22.12	6.42	1.007	1.000
19.58	6.41	1.011	1.000
17.04	6.40	1.015	1.000
14.50	6.23	1.065	.997
13.23	6.06	1.12	.995
11.96	5.76	1.22	.987
10.69	5.37	1.37	.974
9.423	4.92	1.56	.953
8.153	4.48	1.78	.926
6.883	4.02	2.04	.891
5.613	3.56	2.35	.847
4.978	3.33	2.52	.822
4.343	3.12	2.70	.795
3.708	2.92	2.87	.768
3.073	2.67	3.12	.730
2.438	2.48	3.28	.698
1.803	2.26	3.51	.656
1.549	2.18	3.60	.642
1.295	2.09	3.69	.623
1.041	2.01	3.72	.602
.914	1.93	3.77	.582
.787	1.85	3.77	.558
.660	1.76	3.77	.529
.533	1.63	3.79	.493
.432	1.43	3.94	.441
.279	1.12	4.10	.351

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TABLE 67 - Run 57

$M = 6.47$   
 $Re = 12,775$   
 $\frac{Tw}{T} = 4.35$   
 $C_q = 12.1 \times 10^{-4}$   
 $P_o = 35.01 \text{ atm}$   
 $T_t = 549^\circ K$   
 $T = 58.6^\circ K$   
 $U = 993 \text{ m/sec}$

Y (mm)	M	T/T	U/U
29.95	6.47	1.000	1.000
27.41	6.46	1.003	1.000
24.87	6.44	1.009	1.000
22.33	6.43	1.009	.999
19.79	6.42	1.012	.999
17.25	6.32	1.044	.998
15.98	6.18	1.085	.996
14.71	5.95	1.162	.991
13.44	5.63	1.277	.983
12.17	5.31	1.394	.970
10.90	4.81	1.613	.945
9.627	4.34	1.862	.915
8.357	3.91	2.12	.880
7.087	3.48	2.43	.837
5.817	3.06	2.77	.787
4.547	2.67	3.12	.729
3.277	2.30	3.48	.663
2.642	2.13	3.64	.628
2.007	1.92	3.86	.581
1.753	1.85	3.93	.568
1.499	1.76	4.02	.546
1.245	1.70	4.05	.529
.991	1.60	4.13	.501
.864	1.52	4.17	.479
.737	1.43	4.20	.452
.610	1.33	4.21	.424
.483	1.18	4.29	.377
.279	.908	4.33	.292

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3 REPORT TITLE "Characteristics of the Turbulent Boundary Layer with Heat and Mass Transfer: Data Tabulation"		
4 DESCRIPTIVE NOTES (Type of report and inclusive dates) <b>Final</b>		
5 AUTHOR(S) (Last name, first name, initial) Danberg, James E.		
6 REPORT DATE 23 January 1967	7a TOTAL NO OF PAGES 47	7b NO OF REFS 4
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10 AVAILABILITY/LIMITATION NOTICES "Distribution of this document is unlimited."		
11 SUPPLEMENTARY NOTES		12 SPONSORING MILITARY ACTIVITY
13 ABSTRACT A tabulation of turbulent boundary layer data obtained under conditions of heat and mass transfer at a Mach number of 6.7 is presented. The report supplements the treatise given in NOLTR 64-99. A brief description of the model and test procedure is included.		

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14 KEY WORDS	LINK A		LINK B		LINK C	
	ROLE	WT	ROLE	WT	ROLE	WT
1. turbulent boundary layer						
2. heat transfer						
3. mass transfer						
4. hypersonic flow						

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